

US009102802B2

## (12) United States Patent

Leser et al.

(10) Patent No.: US 9,102,802 B2 (45) Date of Patent: Aug. 11, 2015

### (54) POLYMERIC MATERIAL FOR AN INSULATED CONTAINER

(71) Applicant: **BERRY PLASTICS CORPORATION**,

Evansville, IN (US)

(72) Inventors: **Chris K. Leser**, Evansville, IN (US); **Philip A. Driskill**, Newburgh, IN (US);

Charles T. Wallace, Evansville, IN
(US); John B. Euler, Evansville, IN
(US); Jason J. Paladino, Newburgh, IN
(US); Milan C. Maravich, Newburgh,
IN (US); Daniel O. Davis, Cynthiana, IN
(US); Jeffrey A. Mann, Evansville, IN
(US); Randy A. Bowlds, Evansville, IN
(US); Svetlana I. Contrada, Manalapan,

NJ (US)

(73) Assignee: Berry Plastics Corporation, Evansville,

IN (US)

(\*) Notice: Subject to any disclaimer, the term of this

patent is extended or adjusted under 35

U.S.C. 154(b) by 0 days.

(21) Appl. No.: **14/486,618** 

(22) Filed: **Sep. 15, 2014** 

(65) Prior Publication Data

US 2015/0001435 A1 Jan. 1, 2015 **Related U.S. Application Data** 

- (63) Continuation of application No. 13/491,327, filed on Jun. 7, 2012, now Pat. No. 8,883,280.
- (60) Provisional application No. 61/529,632, filed on Aug. 31, 2011, provisional application No. 61/618,604, filed on Mar. 30, 2012.
- (51) Int. Cl. *C08J 9/00 C08L 23/10*

(2006.01) (2006.01)

(Continued)

(52) U.S. Cl.

(Continued)

#### (58) Field of Classification Search

See application file for complete search history.

#### (56) References Cited

#### U.S. PATENT DOCUMENTS

1,396,282 A 11/1921 Penn 1,435,120 A 11/1922 Holman

(Continued)

#### FOREIGN PATENT DOCUMENTS

CA 2291607 6/2000 CA 2765489 12/2010

(Continued)

### OTHER PUBLICATIONS

International Search Report and Written Opinion dated Jan. 19, 2015, relating to International Application No. PCT/US2014/059312.

(Continued)

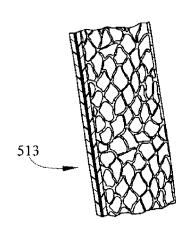
Primary Examiner — Michael C Miggins

(74) Attorney, Agent, or Firm — Barnes & Thornburg LLP

(57) ABSTRACT

A formulation includes a polymeric material, a nucleating agent, a blowing agent, and a surface active agent. The formulation can be used to form a container.

20 Claims, 6 Drawing Sheets



# **US 9,102,802 B2**Page 2

	I-4 Cl		4 0 40 726 4	7/1000	A Itaammin a
(51)	Int. Cl.	(200(-01)	4,940,736 A 5,078,817 A		Alteepping Takagaki
	C08J 9/04	(2006.01)	5,158,986 A	10/1992	
	E04B 1/78	(2006.01)	5,160,674 A	11/1992	
	C08L 23/04	(2006.01)	5,180,751 A	1/1993	
	C08L 23/12	(2006.01)	5,286,428 A		Hayashi
	C08L 23/06	(2006.01)	5,308,568 A 5,348,795 A	5/1994 9/1994	
	C08J 9/06	(2006.01)	5,366,791 A	11/1994	
	C08J 9/12	(2006.01)	5,385,260 A		Gatcomb
	B32B 33/00	(2006.01)	5,443,769 A		Karabedian
	B65D 1/40	(2006.01)	5,445,315 A	8/1995	
	B32B 1/02	(2006.01)	5,490,631 A	2/1996	
	B29D 22/00	(2006.01)	5,547,124 A 5,605,936 A		Mueller DeNicola, Jr.
	B29D 23/00	(2006.01)	5,622,308 A	4/1997	
	B32B 1/08	(2006.01)	5,628,453 A	5/1997	MacLaughlin
	C08L 23/08	(2006.01)	5,629,076 A		Fukasawa
	C08L 23/14	(2006.01)	5,759,624 A	6/1998	
(52)	U.S. Cl.		5,765,710 A 5,766,709 A		Bergerioux Geddes
` /	CPC C08J 9/04 (20	013.01); <i>C08J 9/122</i> (2013.01);	5,769,311 A	6/1998	
		013.01); <i>B29D 22/00</i> (2013.01);	5,819,507 A	10/1998	
		2013.01); <i>B32B 1/02</i> (2013.01);	5,840,139 A	11/1998	
		013.01); <i>B32B 33/00</i> (2013.01);	5,866,053 A	2/1999	
		2013.01); <i>C08J 9/00</i> (2013.01);	5,868,309 A	2/1999 8/1999	
	`	2013.01); <i>C08J 9/12</i> (2013.01);	5,944,225 A 5,948,839 A	9/1999	
		01/03 (2013.01); C08J 2205/04	6,007,437 A	12/1999	
		C08J 2323/04 (2013.01); C08J	6,030,476 A		Geddes
		3.01); <i>C08J 2423/12</i> (2013.01);	6,034,144 A	3/2000	
		013.01); <i>C08L 23/06</i> (2013.01);	6,051,174 A	4/2000	
		013.01); <i>C08L 23/12</i> (2013.01);	6,071,580 A 6,103,153 A	6/2000 8/2000	
		2013.01); <i>E04B 1/78</i> (2013.01);	6,129,653 A		Fredricks
		/139 (2015.01); Y10T 428/1348	6,136,396 A	10/2000	
		710T 428/1376 (2015.01); Y10T	6,139,665 A		Schmelzer
		.01); <i>Y10T 428/1476</i> (2015.01);	6,142,331 A		Breining
	420/1397 (2013	Y10T 428/28 (2015.01),	6,169,122 B1 6,231,942 B1	5/2001	Blizard Blizard
		1101 420/20 (2013.01)	6,235,380 B1	5/2001	
(56)	Dofowo	CI. 1	6 267 927 D1	7/2001	Mitchell
	Keierei	ices Cited	6,267,837 B1		
(30)	Referen	nces Cited	6,284,810 B1	9/2001	Burnham
(50)		DOCUMENTS	6,284,810 B1 6,294,115 B1	9/2001 9/2001	Burnham Blizard
, ,	U.S. PATENT	DOCUMENTS	6,284,810 B1	9/2001	Burnham Blizard Takaoka
	U.S. PATENT 1,920,529 A 8/1933	DOCUMENTS Sidebotham	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1	9/2001 9/2001 10/2001 10/2001 11/2001	Burnham Blizard Takaoka Schmelzer Geddes
, ,	U.S. PATENT 1,920,529 A 8/1933 1,969,030 A 8/1934	DOCUMENTS Sidebotham Page	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,328,916 B1	9/2001 9/2001 10/2001 10/2001 11/2001 12/2001	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa
	U.S. PATENT 1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937	DOCUMENTS Sidebotham Page	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,328,916 B1 6,376,059 B1	9/2001 9/2001 10/2001 10/2001 11/2001 12/2001 4/2002	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson
	U.S. PATENT 1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967	Sidebotham Page Smith Barrington Shapiro	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,328,916 B1 6,376,059 B1 6,379,802 B2	9/2001 9/2001 10/2001 10/2001 11/2001 12/2001 4/2002 4/2002	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito
	U.S. PATENT 1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,327,038 A 6/1967	Sidebotham Page Smith Barrington Shapiro Fox	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,328,916 B1 6,376,059 B1 6,379,802 B2 6,420,024 B1	9/2001 9/2001 10/2001 10/2001 11/2001 12/2001 4/2002	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez
	U.S. PATENT 1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,327,038 A 6/1967 3,344,222 A 9/1967	Sidebotham Page Smith Barrington Shapiro Fox Shapiro	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,328,916 B1 6,376,059 B1 6,379,802 B2 6,420,024 B1 6,444,073 B1 6,468,451 B1	9/2001 9/2001 10/2001 10/2001 11/2001 12/2001 4/2002 4/2002 7/2002 9/2002 10/2002	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez
	U.S. PATENT 1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,327,038 A 6/1967 3,344,222 A 9/1969 3,468,467 A 9/1969	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,328,916 B1 6,376,059 B1 6,379,802 B2 6,420,024 B1 6,444,073 B1 6,468,451 B1 6,472,473 B1	9/2001 9/2001 10/2001 10/2001 11/2001 12/2001 4/2002 4/2002 7/2002 9/2002 10/2002	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems
	U.S. PATENTI 1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,327,038 A 6/1967 3,344,222 A 9/1969 3,547,012 A 12/1970 3,583,624 A 6/1971	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,328,916 B1 6,376,059 B1 6,379,802 B2 6,420,024 B1 6,444,073 B1 6,468,451 B1 6,472,473 B1 RE37,932 E	9/2001 9/2001 10/2001 10/2001 11/2001 11/2001 4/2002 4/2002 7/2002 9/2002 10/2002 10/2002 12/2002	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin
	U.S. PATENTI 1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,327,038 A 6/1967 3,344,222 A 9/1967 3,468,467 A 9/1969 3,547,012 A 12/1970 3,583,624 A 6/1971 3,733,381 A 5/1973	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock Willette	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,328,916 B1 6,376,059 B1 6,379,802 B2 6,420,024 B1 6,444,073 B1 6,468,451 B1 6,472,473 B1 RE37,932 E 6,512,019 B1	9/2001 9/2001 10/2001 10/2001 11/2001 12/2001 4/2002 4/2002 7/2002 9/2002 10/2002 10/2002 1/2003	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin Agarwal
	U.S. PATENT  1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,327,038 A 6/1967 3,3468,467 A 9/1969 3,547,012 A 12/1970 3,583,624 A 6/1971 3,733,381 A 5/1973 3,793,283 A 2/1974	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock Willette Frailey	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,376,059 B1 6,379,802 B2 6,420,024 B1 6,444,073 B1 6,468,451 B1 6,472,473 B1 RE37,932 E 6,512,019 B1 6,521,675 B1 6,541,105 B1	9/2001 9/2001 10/2001 10/2001 11/2001 11/2001 4/2002 4/2002 7/2002 9/2002 10/2002 10/2002 12/2002	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin Agarwal Wu
	U.S. PATENT  1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,344,222 A 9/1967 3,468,467 A 9/1969 3,547,012 A 12/1970 3,583,624 A 6/1971 3,793,283 A 2/1974 3,846,349 A 11/1974	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock Willette Frailey Harada	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,376,059 B1 6,379,802 B2 6,420,024 B1 6,444,073 B1 6,468,451 B1 6,472,473 B1 RE37,932 E 6,512,019 B1 6,521,675 B1 6,541,105 B1 6,541,105 B1 6,562,447 B2	9/2001 9/2001 10/2001 11/2001 11/2001 4/2002 4/2002 7/2002 9/2002 10/2002 12/2002 1/2003 4/2003 5/2003	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin Agarwal Wu Park
	U.S. PATENT  1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,344,222 A 9/1967 3,468,467 A 9/1969 3,547,012 A 12/1970 3,583,624 A 6/1971 3,733,381 A 5/1973 3,793,283 A 2/1974 3,846,349 A 11/1974 3,967,991 A 7/1976	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock Willette Frailey	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,376,059 B1 6,379,802 B2 6,420,024 B1 6,444,073 B1 6,468,451 B1 6,472,473 B1 RE37,932 E 6,512,019 B1 6,521,675 B1 6,541,105 B1 6,562,447 B2 6,565,934 B1	9/2001 9/2001 10/2001 11/2001 11/2001 4/2002 4/2002 7/2002 10/2002 10/2002 12/2002 1/2003 2/2003 5/2003 5/2003	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin Agarwal Wu Park Wu Fredricks
	U.S. PATENTI 1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,327,038 A 6/1967 3,344,222 A 9/1967 3,547,012 A 12/1970 3,583,624 A 6/1971 3,733,381 A 5/1973 3,793,283 A 2/1974 3,846,349 A 11/1974 3,967,991 A 7/1976 3,971,696 A 7/1976 4,049,122 A 9/1977	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock Willette Frailey Harada Shimano Manfredi Maxwell	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,328,916 B1 6,376,059 B1 6,379,802 B2 6,420,024 B1 6,444,073 B1 6,444,473 B1 RE37,932 E 6,512,019 B1 6,521,675 B1 6,521,675 B1 6,541,105 B1 6,562,447 B2 6,565,934 B1 6,586,532 B1	9/2001 9/2001 10/2001 11/2001 11/2001 12/2001 4/2002 4/2002 9/2002 10/2002 10/2002 1/2003 2/2003 4/2003 5/2003 7/2003	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin Agarwal Wu Park Wu Fredricks Gauthy
	U.S. PATENT  1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,344,222 A 9/1967 3,468,467 A 9/1969 3,547,012 A 12/1970 3,583,624 A 6/1971 3,793,283 A 2/1974 3,793,283 A 2/1974 3,846,349 A 11/1974 3,967,991 A 7/1976 4,049,122 A 9/1977 4,070,513 A 1/1978	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock Willette Frailey Harada Shimano Manfredi Maxwell Rhoads	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,376,059 B1 6,379,802 B2 6,420,024 B1 6,444,073 B1 6,468,451 B1 6,472,473 B1 RE37,932 E 6,512,019 B1 6,521,675 B1 6,541,105 B1 6,562,447 B2 6,565,934 B1	9/2001 9/2001 10/2001 11/2001 11/2001 4/2002 4/2002 7/2002 10/2002 10/2002 12/2002 1/2003 2/2003 5/2003 5/2003	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin Agarwal Wu Park Wu Fredricks Gauthy Tau
	U.S. PATENT  1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,344,222 A 9/1967 3,468,467 A 9/1969 3,547,012 A 12/1970 3,583,624 A 6/1971 3,793,283 A 2/1974 3,793,283 A 2/1974 3,846,349 A 11/1974 3,967,991 A 7/1976 3,971,696 A 7/1976 4,070,513 A 1/1978 4,106,397 A 8/1978	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock Willette Frailey Harada Shimano Manfredi Maxwell Rhoads Amberg	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,379,802 B2 6,420,024 B1 6,479,802 B2 6,420,024 B1 6,468,451 B1 6,472,473 B1 RE37,932 E 6,512,019 B1 6,521,675 B1 6,521,675 B1 6,562,447 B2 6,565,934 B1 6,586,532 B1 6,586,532 B1 6,593,005 B2 6,593,384 B2 6,613,811 B1	9/2001 9/2001 10/2001 11/2001 11/2001 4/2002 4/2002 7/2002 10/2002 10/2002 12/2002 1/2003 5/2003 5/2003 5/2003 7/2003 7/2003 9/2003	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin Agarwal Wu Park Wu Fredricks Gauthy Tau Anderson Pallaver
	U.S. PATENT  1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,344,222 A 9/1967 3,468,467 A 9/1969 3,547,012 A 12/1970 3,583,624 A 6/1971 3,733,381 A 5/1973 3,793,283 A 2/1974 3,967,991 A 7/1976 3,971,696 A 7/1976 4,049,122 A 9/1977 4,106,397 A 8/1978 4,171,085 A 10/1979	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock Willette Frailey Harada Shimano Manfredi Maxwell Rhoads Amberg Doty	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,376,059 B1 6,379,802 B2 6,420,024 B1 6,444,073 B1 6,468,451 B1 6,472,473 B1 RE37,932 E 6,512,019 B1 6,521,675 B1 6,521,675 B1 6,562,447 B2 6,565,934 B1 6,586,532 B1 6,593,005 B2 6,593,384 B2 6,613,811 B1 6,616,434 B1	9/2001 9/2001 10/2001 11/2001 11/2001 4/2002 4/2002 7/2002 10/2002 10/2002 12/2002 1/2003 4/2003 5/2003 5/2003 7/2003 7/2003 9/2003 9/2003	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin Agarwal Wu Prark Wu Fredricks Gauthy Tau Anderson Pallaver Burnham
	U.S. PATENTI 1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,327,038 A 6/1967 3,344,222 A 9/1967 3,547,012 A 12/1970 3,583,624 A 6/1971 3,733,381 A 5/1973 3,793,283 A 2/1974 3,846,349 A 11/1974 3,967,991 A 7/1976 4,049,122 A 9/1977 4,070,513 A 1/1978 4,106,397 A 8/1978 4,117,085 A 10/1979 4,197,948 A 4/1980 4,240,568 A 12/1980	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock Willette Frailey Harada Shimano Manfredi Maxwell Rhoads Amberg Doty Amberg Pool	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,376,059 B1 6,379,802 B2 6,420,024 B1 6,444,073 B1 6,468,451 B1 6,472,473 B1 RE37,932 E 6,512,019 B1 6,521,675 B1 6,541,105 B1 6,562,447 B2 6,565,934 B1 6,562,447 B2 6,565,934 B1 6,586,532 B1 6,593,005 B2 6,593,384 B2 6,613,811 B1 6,616,434 B1 6,646,019 B2	9/2001 9/2001 10/2001 11/2001 11/2001 12/2001 4/2002 4/2002 9/2002 10/2002 10/2002 12/2003 4/2003 5/2003 7/2003 7/2003 7/2003 9/2003 9/2003 11/2003	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin Agarwal Wu Park Wu Park Wu Tau Anderson Pallaver Burnham Perez
	U.S. PATENT  1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,344,222 A 9/1967 3,468,467 A 9/1969 3,547,012 A 12/1970 3,583,624 A 6/1971 3,793,283 A 2/1974 3,793,283 A 2/1974 3,846,349 A 11/1974 3,967,991 A 7/1976 3,971,696 A 7/1976 4,049,122 A 9/1977 4,070,513 A 1/1978 4,106,397 A 8/1978 4,117,085 A 10/1979 4,197,948 A 4/1980 4,226,268 A 8/1981	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock Willette Frailey Harada Shimano Manfredi Maxwell Rhoads Amberg Doty Amberg Pool Herbst	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,376,059 B1 6,379,802 B2 6,420,024 B1 6,444,073 B1 6,468,451 B1 6,472,473 B1 RE37,932 E 6,512,019 B1 6,521,675 B1 6,521,675 B1 6,562,447 B2 6,565,934 B1 6,586,532 B1 6,593,005 B2 6,593,384 B2 6,613,811 B1 6,616,434 B1	9/2001 9/2001 10/2001 11/2001 11/2001 4/2002 4/2002 7/2002 10/2002 10/2002 12/2002 1/2003 4/2003 5/2003 5/2003 7/2003 7/2003 9/2003 9/2003	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin Agarwal Wu Park Wu Fredricks Gauthy Tau Anderson Pallaver Burnham Perez Read
	U.S. PATENT  1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,342,222 A 9/1967 3,468,467 A 9/1969 3,547,012 A 12/1970 3,583,624 A 6/1971 3,793,283 A 2/1974 3,793,283 A 2/1974 3,971,696 A 7/1976 4,049,122 A 9/1977 4,070,513 A 1/1978 4,110,085 A 10/1979 4,110,085 A 10/1979 4,111,085 A 12/1980 4,240,568 A 12/1980 4,284,226 A 8/1981	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock Willette Frailey Harada Shimano Manfredi Maxwell Rhoads Amberg Doty Amberg Pool Herbst Mueller	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,379,802 B2 6,420,024 B1 6,464,4073 B1 6,468,451 B1 6,472,473 B1 RE37,932 E 6,512,019 B1 6,541,105 B1 6,562,447 B2 6,565,934 B1 6,586,532 B1 6,593,005 B2 6,593,384 B2 6,613,811 B1 6,616,434 B1 6,646,019 B2 6,649,666 B1 6,713,139 B2 6,720,362 B1	9/2001 9/2001 10/2001 11/2001 11/2001 4/2002 4/2002 7/2002 10/2002 10/2002 12/2002 1/2003 5/2003 5/2003 7/2003 7/2003 9/2003 9/2003 11/2003 11/2003 11/2003 3/2004 4/2004	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin Agarwal Wu Park Wu Fredricks Gauthy Tau Anderson Pallaver Burnham Perez Read Usui Park
	U.S. PATENT  1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,344,222 A 9/1967 3,468,467 A 9/1969 3,547,012 A 12/1970 3,583,624 A 6/1971 3,733,381 A 5/1973 3,793,283 A 2/1974 3,967,991 A 7/1976 3,971,696 A 7/1976 4,049,122 A 9/1977 4,107,513 A 1/1978 4,171,085 A 10/1979 4,197,948 A 4/1980 4,284,226 A 8/1981 4,298,331 A 11/1981 4,299,349 A 11/1981	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock Willette Frailey Harada Shimano Manfredi Maxwell Rhoads Amberg Doty Amberg Pool Herbst Mueller Gilden	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,379,802 B2 6,420,024 B1 6,468,451 B1 6,472,473 B1 RE37,932 E 6,512,019 B1 6,521,675 B1 6,521,675 B1 6,562,447 B2 6,565,934 B1 6,586,532 B1 6,586,532 B1 6,593,085 B2 6,613,811 B1 6,616,434 B1 6,646,019 B2 6,649,666 B1 6,713,139 B2 6,720,362 B1 6,749,913 B2	9/2001 9/2001 10/2001 11/2001 11/2001 4/2002 4/2002 7/2002 10/2002 10/2002 12/2002 1/2003 5/2003 5/2003 7/2003 7/2003 9/2003 9/2003 11/2003 11/2003 3/2004 4/2004 6/2004	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin Agarwal Wu Park Wu Fredricks Gauthy Tau Anderson Pallaver Burnham Perez Read Usui Park Wu Lsui Park Watanabe
	U.S. PATENT  1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,344,222 A 9/1967 3,547,012 A 12/1970 3,583,624 A 6/1971 3,793,283 A 2/1974 3,793,283 A 2/1974 3,846,349 A 11/1974 3,967,991 A 7/1976 3,971,696 A 7/1976 3,971,696 A 7/1976 4,049,122 A 9/1977 4,070,513 A 1/1787 4,106,397 A 8/1978 4,171,085 A 10/1979 4,197,948 A 4/1980 4,284,226 A 8/1981 4,298,331 A 11/1981 4,299,349 A 11/1981 4,300,891 A 11/1981	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock Willette Frailey Harada Shimano Manfredi Maxwell Rhoads Amberg Doty Amberg Pool Herbst Mueller	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,376,059 B1 6,379,802 B2 6,420,024 B1 6,444,073 B1 6,468,451 B1 6,472,473 B1 RE37,932 E 6,512,019 B1 6,521,675 B1 6,541,105 B1 6,562,447 B2 6,565,934 B1 6,586,532 B1 6,593,005 B2 6,593,814 B2 6,613,811 B1 6,616,434 B1 6,646,019 B2 6,649,666 B1 6,713,139 B2 6,720,362 B1 6,749,913 B2 6,779,662 B2	9/2001 9/2001 10/2001 11/2001 11/2001 4/2002 4/2002 7/2002 10/2002 10/2002 12/2002 1/2003 4/2003 5/2003 5/2003 7/2003 7/2003 9/2003 11/2003 11/2003 11/2003 3/2004 4/2004 8/2004	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin Agarwal Wu Fredricks Gauthy Tau Anderson Pallaver Burnham Perez Read Usui Park Watanabe Dorsey
	U.S. PATENT  1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,344,222 A 9/1967 3,468,467 A 9/1969 3,547,012 A 12/1970 3,583,624 A 6/1971 3,793,283 A 2/1974 3,793,283 A 2/1974 3,846,349 A 11/1974 3,967,991 A 7/1976 3,971,696 A 7/1976 4,049,122 A 9/1977 4,070,513 A 1/1978 4,106,397 A 8/1978 4,117,085 A 10/1979 4,117,085 A 10/1979 4,117,085 A 10/1979 4,117,085 A 10/1979 4,117,085 A 11/1981 4,240,568 A 12/1980 4,284,226 A 8/1981 4,298,331 A 11/1981 4,300,891 A 11/1981 4,300,891 A 11/1981 4,349,400 A 9/1982 4,365,460 A 12/1982	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock Willette Frailey Harada Shimano Manfredi Maxwell Rhoads Amberg Doty Amberg Pool Herbst Mueller Gilden Bemiss Gilden Cress	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,379,802 B2 6,420,024 B1 6,444,073 B1 6,468,451 B1 6,472,473 B1 RE37,932 E 6,512,019 B1 6,521,675 B1 6,541,105 B1 6,562,447 B2 6,565,934 B1 6,565,934 B1 6,565,934 B1 6,566,434 B1 6,616,434 B1 6,616,434 B1 6,646,019 B2 6,649,666 B1 6,713,139 B2 6,720,362 B1 6,720,362 B1 6,749,913 B2 6,779,662 B2 6,811,843 B2	9/2001 9/2001 10/2001 11/2001 11/2001 11/2001 4/2002 4/2002 9/2002 10/2002 10/2002 12/2003 4/2003 5/2003 5/2003 7/2003 7/2003 9/2003 11/2003 11/2003 3/2004 4/2004 6/2004 8/2004	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin Agarwal Wu Park Wu Fredricks Gauthy Tau Anderson Pallaver Burnham Perez Read Usui Park Watanabe Dorsey DeBraal
	U.S. PATENT  1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,344,222 A 9/1967 3,468,467 A 9/1969 3,547,012 A 12/1970 3,583,624 A 6/1971 3,793,283 A 2/1974 3,793,283 A 2/1974 3,967,991 A 7/1976 4,049,122 A 9/1977 4,070,513 A 1/1981 4,171,085 A 10/1979 4,117,948 A 4/1980 4,240,568 A 12/1980 4,284,226 A 8/1981 4,298,331 A 11/1981 4,299,349 A 11/1981 4,349,400 A 9/1982 4,365,460 A 12/1982 4,409,045 A 10/1983	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock Willette Frailey Harada Shimano Manfredi Maxwell Rhoads Amberg Doty Amberg Pool Herbst Mueller Gilden Bemiss Gilden Cress Busse	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,379,802 B2 6,420,024 B1 6,444,073 B1 6,468,451 B1 6,472,473 B1 RE37,932 E 6,512,019 B1 6,521,675 B1 6,541,105 B1 6,565,934 B1 6,565,934 B1 6,565,934 B1 6,566,32 B1 6,593,005 B2 6,593,384 B2 6,613,811 B1 6,616,434 B1 6,646,019 B2 6,649,666 B1 6,713,139 B2 6,720,362 B1 6,749,913 B2 6,779,662 B2 6,811,843 B2 6,811,843 B2 6,814,253 B2	9/2001 9/2001 10/2001 11/2001 11/2001 11/2001 4/2002 4/2002 9/2002 10/2002 10/2002 12/2003 4/2003 5/2003 5/2003 7/2003 7/2003 9/2003 11/2003 11/2003 11/2003 11/2003 11/2004 4/2004 6/2004 8/2004 11/2004	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin Agarwal Wu Park Wu Fredricks Gauthy Tau Anderson Pallaver Burnham Perez Read Usui Park Watanabe Dorsey DeBraal Wong
	U.S. PATENT  1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,344,222 A 9/1967 3,468,467 A 9/1969 3,547,012 A 12/1970 3,583,624 A 6/1971 3,793,283 A 2/1974 3,793,283 A 2/1974 3,967,991 A 7/1976 3,971,696 A 7/1976 4,049,122 A 9/1977 4,070,513 A 1/1978 4,106,397 A 8/1978 4,171,085 A 10/1979 4,197,948 A 4/1980 4,284,226 A 8/1981 4,298,331 A 11/1981 4,299,349 A 11/1981 4,300,891 A 11/1981 4,300,891 A 11/1981 4,365,460 A 9/1982 4,469,045 A 10/1983 4,4550,046 A 10/1983	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock Willette Frailey Harada Shimano Manfredi Maxwell Rhoads Amberg Doty Amberg Pool Herbst Mueller Gilden Bemiss Gilden Cress Busse Miller	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,379,802 B2 6,420,024 B1 6,444,073 B1 6,468,451 B1 6,472,473 B1 RE37,932 E 6,512,019 B1 6,521,675 B1 6,541,105 B1 6,562,447 B2 6,565,934 B1 6,565,934 B1 6,565,934 B1 6,566,434 B1 6,616,434 B1 6,616,434 B1 6,646,019 B2 6,649,666 B1 6,713,139 B2 6,720,362 B1 6,720,362 B1 6,749,913 B2 6,779,662 B2 6,811,843 B2	9/2001 9/2001 10/2001 11/2001 11/2001 12/2001 4/2002 7/2002 9/2002 10/2002 10/2002 12/2003 4/2003 5/2003 5/2003 7/2003 7/2003 9/2003 9/2003 11/2003 11/2003 3/2004 4/2004 6/2004 8/2004 11/2004 4/2004 4/2005	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin Agarwal Wu Park Wu Fredricks Gauthy Tau Anderson Pallaver Burnham Perez Read Usui Park Watanabe Dorsey DeBraal
	U.S. PATENT  1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,344,222 A 9/1967 3,547,012 A 12/1970 3,583,624 A 6/1971 3,793,283 A 2/1974 3,793,283 A 2/1974 3,846,349 A 11/1974 3,967,991 A 7/1976 3,971,696 A 7/1976 3,971,696 A 7/1976 4,049,122 A 9/1977 4,070,513 A 1/1978 4,106,397 A 8/1978 4,171,085 A 10/1979 4,197,948 A 4/1980 4,240,568 A 12/1980 4,240,568 A 12/1980 4,240,568 A 12/1981 4,298,331 A 11/1981 4,300,891 A 11/1981 4,300,891 A 11/1981 4,300,891 A 11/1981 4,300,891 A 11/1981 4,365,460 A 12/1982 4,409,045 A 10/1983 4,550,046 A 10/1983 4,550,046 A 10/1983 4,550,046 A 10/1983	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock Willette Frailey Harada Shimano Manfredi Maxwell Rhoads Amberg Doty Amberg Pool Herbst Mueller Gilden Bemiss Gilden Cress Busse	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,379,802 B2 6,420,024 B1 6,464,073 B1 6,468,451 B1 6,472,473 B1 RE37,932 E 6,512,019 B1 6,541,105 B1 6,541,105 B1 6,562,447 B2 6,565,934 B1 6,586,532 B1 6,593,005 B2 6,593,384 B2 6,613,811 B1 6,616,434 B1 6,646,019 B2 6,649,666 B1 6,713,139 B2 6,720,362 B1 6,749,913 B2 6,749,913 B2 6,779,662 B2 6,811,843 B2 6,814,253 B2 6,884,377 B1 6,884,851 B2	9/2001 9/2001 10/2001 11/2001 11/2001 4/2002 4/2002 7/2002 10/2002 10/2002 10/2002 12/2003 4/2003 5/2003 5/2003 5/2003 7/2003 9/2003 9/2003 11/2003 11/2003 11/2004 4/2004 6/2004 8/2004 11/2004 11/2004 4/2005 4/2005	Burnham Blizard Takaoka Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin Agarwal Wu Park Wu Fredricks Gauthy Tau Anderson Pallaver Burnham Perez Read Usui Park Watanabe Dorsey DeBraal Wong Goeking Burnham Gauthy
	U.S. PATENT  1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,344,222 A 9/1967 3,468,467 A 9/1969 3,547,012 A 12/1970 3,583,624 A 6/1971 3,793,283 A 2/1974 3,793,283 A 2/1974 3,846,349 A 11/1974 3,967,991 A 7/1976 3,971,696 A 7/1976 4,049,122 A 9/1977 4,070,513 A 1/1978 4,106,397 A 8/1978 4,117,085 A 10/1979 4,117,085 A 10/1979 4,117,085 A 10/1979 4,117,085 A 10/1979 4,117,085 A 11/1981 4,298,331 A 11/1981 4,298,331 A 11/1981 4,300,891 A 11/1981 4,300,891 A 11/1981 4,300,891 A 11/1981 4,349,400 A 9/1982 4,4621,763 A 10/1983 4,550,046 A 10/1983 4,706,873 A 11/1987 4,720,023 A 1/1988	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock Willette Frailey Harada Shimano Manfredi Maxwell Rhoads Amberg Doty Amberg Pool Herbst Mueller Gilden Bemiss Gilden Cress Busse Miller Brauner Schulz Jeff	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,376,059 B1 6,379,802 B2 6,420,024 B1 6,444,073 B1 6,468,451 B1 6,472,473 B1 RE37,932 E 6,512,019 B1 6,521,675 B1 6,541,105 B1 6,562,447 B2 6,565,934 B1 6,586,532 B1 6,593,005 B2 6,593,384 B2 6,613,811 B1 6,616,434 B1 6,646,019 B2 6,649,666 B1 6,713,139 B2 6,720,362 B1 6,749,913 B2 6,779,662 B2 6,811,843 B2 6,814,253 B2 6,884,377 B1 6,884,851 B2 6,908,651 B2	9/2001 9/2001 10/2001 11/2001 11/2001 11/2001 4/2002 4/2002 9/2002 10/2002 10/2002 11/2003 2/2003 4/2003 5/2003 7/2003 7/2003 7/2003 7/2003 9/2003 11/2003 11/2003 11/2004 4/2004 4/2004 4/2004 4/2005 4/2005 4/2005 6/2005	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin Agarwal Wu Park Wu Park Wu Tau Anderson Pallaver Burnham Perez Read Usui Park Watanabe Dorsey DeBraal Wong Goeking Burnham Gauthy Watanabe
	U.S. PATENT  1,920,529 A 8/1933 1,969,030 A 8/1934 2,097,899 A 11/1937 2,809,776 A 10/1957 3,312,383 A 4/1967 3,344,222 A 9/1967 3,468,467 A 9/1969 3,547,012 A 12/1970 3,583,624 A 6/1971 3,733,381 A 5/1973 3,793,283 A 2/1974 3,793,283 A 2/1974 3,846,349 A 11/1974 4,070,513 A 1/1978 4,1070,513 A 1/1980 4,240,568 A 12/1980 4,240,568 A 11/1981 4,300,891 A 11/1981 4,300,891 A 11/1981 4,349,400 A 9/1982 4,365,460 A 12/1982 4,4550,046 A 10/1983 4,550,046 A 10/1983 4,550,046 A 11/1986 4,706,873 A 11/1987	Sidebotham Page Smith Barrington Shapiro Fox Shapiro Amberg Amberg Peacock Willette Frailey Harada Shimano Manfredi Maxwell Rhoads Amberg Doty Amberg Pool Herbst Mueller Gilden Bemiss Gilden Cress Busse Miller Brauner Schulz Jeff Schubert	6,284,810 B1 6,294,115 B1 6,306,973 B1 6,308,883 B1 6,319,590 B1 6,379,802 B2 6,420,024 B1 6,464,073 B1 6,468,451 B1 6,472,473 B1 RE37,932 E 6,512,019 B1 6,541,105 B1 6,541,105 B1 6,562,447 B2 6,565,934 B1 6,586,532 B1 6,593,005 B2 6,593,384 B2 6,613,811 B1 6,616,434 B1 6,646,019 B2 6,649,666 B1 6,713,139 B2 6,720,362 B1 6,749,913 B2 6,749,913 B2 6,779,662 B2 6,811,843 B2 6,814,253 B2 6,884,377 B1 6,884,851 B2	9/2001 9/2001 10/2001 11/2001 11/2001 11/2001 4/2002 4/2002 9/2002 10/2002 10/2002 11/2003 2/2003 4/2003 5/2003 7/2003 7/2003 7/2003 7/2003 9/2003 11/2003 11/2003 11/2004 4/2004 4/2004 4/2004 4/2005 4/2005 4/2005 6/2005	Burnham Blizard Takaoka Schmelzer Geddes Nishikawa Anderson Ito Perez Reeves Perez Ansems Baldwin Agarwal Wu Park Wu Park Wu Tau Anderson Pallaver Burnham Perez Read Usui Park Watanabe Dorsey DeBraal Wong Goeking Burnham Gauthy Watanabe Cardona

# US 9,102,802 B2 Page 3

(56)			Referen	ces Cited	8,067,319		11/2011	
	Ţ	LS. P	PATENT	DOCUMENTS	8,076,381 8,076,416		12/2011	Miyagawa Ellul
	`	0.0.1		DOCOMENTS	8,084,537		12/2011	
	7,070,852		7/2006		8,087,147		1/2012	
	7,074,466 1 7,094,463 1		7/2006 8/2006	DeBraal	8,105,459 8,119,237		2/2012	Alvarez Peng
	7,121,991			Mannlein	8,124,234	B2	2/2012	Weaver
	7,144,532		12/2006		8,173,233		5/2012	
	7,173,069			Swennen	8,198,374 8,211,982		6/2012 7/2012	
	7,234,629 1 7,281,650 1		6/2007 10/2007		8,227,075			Matsushita
	7,355,089		4/2008		8,273,068		9/2012	Chang
	7,361,720		4/2008	Pierini	8,273,826 8,273,838		9/2012 9/2012	
	7,365,136 I 7,423,071 I			Huovinen Mogami	8,288,470		10/2012	
	7,458,504			Robertson	8,304,496	B2	11/2012	
	7,504,347		3/2009		8,404,780 8,435,615		3/2013	Weaver Tsuchida
	7,510,098 I 7,513,386 I		3/2009 4/2009		8,679,620			Matsushita
	7,513,580		4/2009		2001/0010849	A1	8/2001	Blizard
	7,524,911	B2	4/2009	Karjala	2002/0030296		3/2002	
	7,557,147 [ 7,579,408 ]		7/2009 8/2009	Martinez	2002/0058126 2002/0137851		9/2002	Kannankeril Kim
	7,582,716		9/2009		2002/0144769		10/2002	
	7,585,557			Aylward	2002/0172818		11/2002	
	7,592,397			Markovich	2003/0003251 2003/0017284			DeBraal Watanabe
	7,608,668 I 7,622,179 I		10/2009 11/2009		2003/0017284		2/2003	
	7,622,529		11/2009		2003/0108695		6/2003	
	7,629,416		12/2009		2003/0138515 2003/0211310		7/2003 11/2003	Harfmann
	7,655,296 I 7,662,881 I		2/2010 2/2010		2003/0211310			Gervasio
	7,666,918		2/2010		2003/0232210	A1	12/2003	Haas
	7,671,106	B2	3/2010	Markovich	2004/0031714		2/2004	
	7,671,131		3/2010 3/2010		2004/0038018 2004/0115418			Anderson Anderson
	7,673,564 I 7,687,442 I		3/2010		2004/0170814		9/2004	VanHandel
	7,695,812	B2	4/2010	Peng	2005/0003122			Debraal
	7,714,071		5/2010		2005/0006449 2005/0101926		5/2005	DAmato Ausen
	7,732,052 I 7,737,061 I		6/2010 6/2010		2005/0104365		5/2005	
	7,737,215		6/2010		2005/0121457		6/2005	
	7,741,397		6/2010		2005/0147807 2005/0159496			Haas Bambara
	7,754,814 I 7,759,404 I		7/2010 7/2010		2005/0184136			Baynum, III
	7,786,216	B2		Soediono	2005/0236294		10/2005	
	7,795,321		9/2010		2005/0256215 2005/0272858			Burnham Pierini
	7,803,728 I 7,811,644 I		9/2010 10/2010		2005/02728383			Haas
	7,818,866		10/2010		2006/0000882			Darzinskas
	7,820,282		10/2010		2006/0095151 2006/0135699		5/2006 6/2006	Mannlein Li
	7,841,974 1 7,842,770 1		11/2010 11/2010		2006/0148920			Musgrave
	7,858,706		12/2010		2006/0178478	A1	8/2006	Ellul
	7,863,379		1/2011		2006/0198983 2006/0199006		9/2006 9/2006	
	7,883,769 I 7,893,166 I		2/2011 2/2011		2006/0199030		9/2006	
	7,897,689		3/2011		2006/0199744		9/2006	
	7,906,587		3/2011		2006/0199872 2006/0199884		9/2006 9/2006	
	7,910,658 I 7,915,192 I		3/2011 3/2011		2006/0199887		9/2006	
	7,918,005	B2	4/2011		2006/0199896		9/2006	
	7,918,016		4/2011		2006/0199897 2006/0199905		9/2006 9/2006	Karjala
	7,922,071 1 7,928,162 1		4/2011 4/2011	Robertson	2006/0199906		9/2006	
	7,935,740		5/2011		2006/0199907	A1	9/2006	Chang
	7,947,367		5/2011		2006/0199908		9/2006	Cheung
	7,951,882 I 7,977,397 I		5/2011 7/2011		2006/0199910 2006/0199911		9/2006 9/2006	Walton Markovich
	7,989,543		8/2011		2006/0199912			Fuchs
	7,993,254	B2	8/2011	Robertson	2006/0199914			Harris
	7,998,579		8/2011		2006/0199930		9/2006	Shan
	7,998,728 I 8,003,176 I		8/2011 8/2011		2006/0199931 2006/0199933		9/2006 9/2006	Poon Okamoto
	8,003,744			Okamoto	2006/0205833			Martinez
	8,012,550	B2	9/2011	Ylitalo	2006/0211819			Hoenig
	8,026,291		9/2011		2006/0234033 2006/0289609			Nishikawa Eritz
	8,043,695	132	10/2011	Dallaru	Z000/0Z <b>8</b> 9009	AI	12/2006	THE

# US 9,102,802 B2 Page 4

(56)	Re	eferen	ces Cited		0108714 A		2 Wittner
	IIS PAT	FENT	DOCUMENTS		(0108741 A (0108743 A		2 Wu 2 Krishnaswamy
	U.S. 171	LEIVI	DOCUMENTS		0125926 A		2 Iyori
2006/0289610	A1 12	/2006	Kling		0132699 A		2 Mann
2007/0010616	A1 1	/2007	Kapur		0178896 A		2 Bastioli 2 Lake
2007/0032600			Mogami Holcomb		(0184657 A (0193365 A		2 Humphries
2007/0056964 2007/0065615		/2007 /2007			0199278 A		2 Lee
2007/0066756		/2007			0199641 A		2 Hsieh
2007/0078222			Chang		0214890 A		2 Senda
2007/0095837			Meier		(0220730 A (0225961 A		2 Li 2 VanHorn
2007/0112127 2007/0141188		/2007	Soediono Kim		0237734 A		2 Maurer
2007/0155900			Chang		0267368 A		2 Wu
2007/0167315			Arriola		(0270039 A (0295994 A		2 Tynys 2 Bernreitner
2007/0167575 2007/0167578			Weaver Arriola		0293994 A		2 Leser
2007/0107378		/2007			0318807 A		2 Leser
2007/0219334	A1 9	/2007	Shan		0023598 A		3 Song
2008/0118738			Boyer		(0032963 A (0052385 A		3 Tokiwa 3 Leser
2008/0121681 2008/0156857			Wiedmeyer Johnston		0032383 A		3 Buehring
2008/0177242			Chang		0303645 A		3 Dix
2008/0227877	A1 9	/2008	Stadlbauer				
2008/0234435			Chang		FOR	EIGN PAT	ENT DOCUMENTS
2008/0260996 2008/0269388			Heilman Markovich	CNI		1200427	2/2001
2008/0280517			Chang	CN CN		1288427 1429309	3/2001 5/2009
2008/0281037			Karjala	DE		1 <del>4</del> 29309 2831240 С	3/1988
2008/0311812 2009/0042472		/2008 /2009	Arriola	DE		6025612 A	
2009/0042472			Yoshida	EP		0086869	8/1983
2009/0069523	A1 3	/2009	Itakura	EP EP		0161597 0318167	11/1985 5/1989
2009/0076216		/2009		EP		0570221	11/1993
2009/0105417 2009/0110944			Walton Aguirre	EP		0659647	6/1995
2009/0170679			Hartjes	EP EP		0972727 0796199	1/2000 2/2001
2009/0220711	A1 9	/2009	Chang	EP		0940240	10/2002
2009/0247033 2009/0263645		/2009		EP		1308263	5/2003
2009/0203043			Barger Weaver	EP		1479716	11/2004
2009/0324914			Lieng	EP EP		1666530 1754744	6/2006 2/2007
2010/0025073			Fagrell	EP		1921023 A	
2010/0028568 2010/0029827			Weaver Ansems	EP		1939099	7/2008
2010/0040818			Farha	EP EP		2266894 2386584 A	12/2010 1 11/2011
2010/0055358			Weaver	GB		2380384 A 1078326	8/1967
2010/0069574 2010/0093942		/2010 /2010		JP		2123043 U	
2010/0093942			Chang	JP		8029618	2/1983
2010/0168267	A1 7.	/2010	Dang	JP JP		3140847 P310847	1/1994 12/2000
2010/0181328		/2010		JP		1310429	11/2001
2010/0181370 2010/0196610			Berbert Chang	JP		3292663	10/2003
2010/0240818	A1 9	/2010	Walton	JP JP		4018101 4168421 A	1/2004 6/2004
2010/0279571		/2010		JP		6096390	4/2006
2010/0324202 2011/0003929			Bafna Soediono	JP		6130814 A	5/2006
2011/0003525		/2011		JP JP		9066856 A 9190756 A	4/2009 8/2009
2011/0009513	A1 1	/2011	Chaudhary	KR		9190730 A 0306320	10/2001
2011/0091688			Maurer	KR		3036558	5/2003
2011/0104414 2011/0111150			Onodera Matsuzaki	KR		4017234	2/2004
2011/0118370		/2011		KR WO		1196666 9413460	11/2012 6/1994
2011/0118416			Arriola	wo		9729150	8/1997
2011/0124818 2011/0136959			Arriola Brandstetter	WO	9	9816575	4/1998
2011/0130939			Harris	WO		0119733 0132758	3/2001 5/2001
2011/0217492	A1 9	/2011	Stamatiou	WO WO		01 <i>327</i> 58 0153079	5/2001 7/2001
2011/0229693			Maurer	WO	0:	3076497	9/2003
2011/0230108 2011/0318560		/2011 /2011	Arriola Yun	WO		3099913	12/2003
2012/0004087			Tharayil	WO WO		4104075 6042908	12/2004 4/2006
2012/0024873	A1 2	/2012	Roseblade	WO		6124369	11/2006
2012/0028065			Bafna	WO	200	7020074	2/2007
2012/0041148 2012/0043374			Bafna Lemon	WO WO		8030953 8038750	3/2008 4/2008
2012/0045574			Zerafati	WO		8038730 8045944	4/2008
	_		-	-			

(56)	References Cited		
	FOREIGN PATE	NT DOCUMENTS	
WO	2008057878	5/2008	
WO	2008080111	7/2008	
WO	2009035580	3/2009	
WO	2010006272	1/2010	
WO	2010019146	2/2010	
WO	2010076701 A1	7/2010	
WO	2010111869	10/2010	
WO	2011005856	1/2011	
WO	2011036272 A2	3/2011	
WO	2011076637	6/2011	
WO	2011141044	11/2011	
WO	2012020106	2/2012	
WO	2012025584	3/2012	
WO	2012044730	4/2012	
WO	2012055797	5/2012	
WO	2012099682	7/2012	

#### OTHER PUBLICATIONS

International Search Report dated Jan. 19, 2015, relating to International Application No. PCT/US2014/059216.

Office Action dated Feb. 2, 2015 for U.S. Appl. No. 14/106,114. Office Action dated Jan. 6, 2015 for Chinese Application No. 201280034350.9 (11 pages).

Office Action dated Jan. 9, 2015 for Chinese Application No. 201280035667.4 (22 pages).

Spanish Search Report of Application No. 201390099, dated Feb. 9, 2015

Borealis AG, DAPLOY(TM) HMS Polypropylene for Foam Extrusion, 2010, 20 pages.

International Search Report and Written Opinion dated Apr. 16, 2014, relating to International Application No. PCT/US2013/075013.

International Search Report and Written Opinion dated Apr. 21, 2014, relating to International Application No. PCT/US2013/074032

International Search Report and Written Opinion dated Apr. 22, 2014, relating to PCT/US2013/074965.

International Search Report and Written Opinion dated Apr. 25, 2014, relating to PCT/US2013/075052.

International Search Report and Written Opinion dated Jul. 3, 2014, relating to International Application No. PCT/US2014/025697.

International Search Report and Written Opinion dated Sep. 17, 2013, relating to International Application No. PCT/US2012/041395.

International Search Report dated Feb. 26, 2013, relating to International Application No. PCT/US2012/043018.

International Search Report dated Jan. 29, 2013, relating to International Application No. PCT/US2012/043017.

International Search Report dated Jan. 30, 2013, relating to International Application No. PCT/US2012/042737.

International Search Report dated Jul. 29, 2013, relating to International Application No. PCT/US2012/043016, 25 pages.

International Search Report dated Jul. 30, 2012, relating to International Application No. PCT/US2012/041397.

International Search Report dated Mar. 11, 2014, relating to International Application No. PCT/US2013/66811.

International Search Report dated Nov. 19, 2012, relating to International Application No. PCT/US2012/041395.

Jaakko I. Raukola, A New Technology to Manufacture Polypropylene Foam Sheet and Biaxially Oriented Foam Film, VTT Publications 361, Technical Research Centre of Finland, Apr. 1998, 100 pages

Machine English translation of JP 2006-130814.

Office action dated Apr. 11, 2014 for U.S. Appl. No. 13/526,417.

Office Action dated Aug. 21, 2014 for U.S. Appl. No. 13/526,454. Office Action dated Jul. 25, 2014 for U.S. Appl. No. 13/525,640.

Office Action dated Sep. 25, 2014 for U.S. Appl. No. 13/526,417.

Office Action dated Oct. 10, 2014 for U.S. Appl. No. 14/106,358.

Office Action dated Oct. 16, 2014 for U.S. Appl. No. 14/106,212. Office Action dated Aug. 19, 2014 for Chinese Application No.

201280035667.4. European Search Report of Application No. 12861450.0, dated Nov.

International Search Report dated Nov. 7, 2014, relating to International Application No. PCT/US2014/51508.

New Zealand First Examination Report for Application No. 619616 dated Oct. 10, 2014.

New Zealand First Examination Report for Application No. 621219 dated Nov. 17, 2014.

Third-Party Submission Under 37 CFR 1.290 filed on Dec. 9, 2014 in U.S. Appl. No. 14/063,252.

Machine English translation of EP0086869.

Singapore Office Action dated Dec. 18, 2014 for Singapore Application No. 2014002273.

Third-Party Submission Under 37 CFR 1.290 filed on Feb. 26, 2015 in U.S. Appl. No. 13/491,007.

Certified English translation of EP0086869.

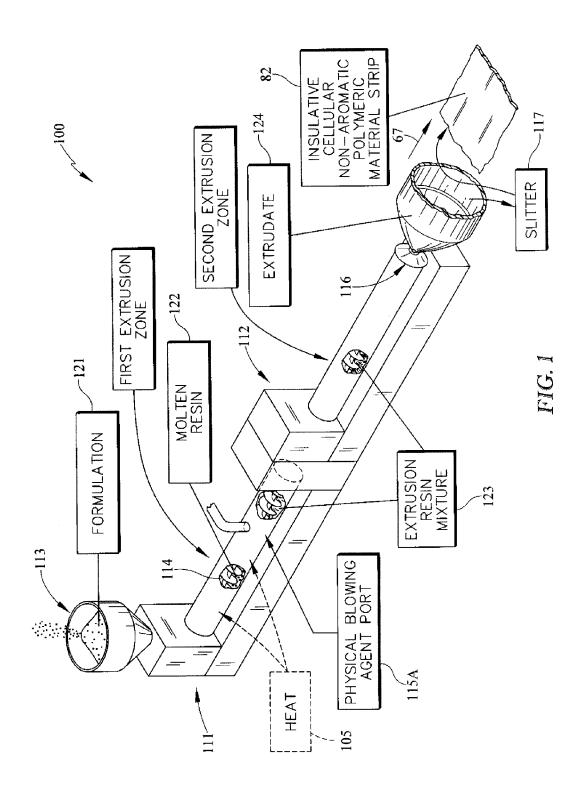
Office Action dated Apr. 30, 2015 for U.S. Appl. No. 14/462,073.

Office Action dated Apr. 14, 2015 for U.S. Appl. No. 14/106,212.

Office Action dated Apr. 10, 2015 for U.S. Appl. No. 14/106,358. English translation of Spanish Search Report of Application No. 201490025, dated Apr. 20, 2015.

Spanish Search Report for Application No. 201490025, dated Apr. 20, 2015.

Office Action dated Jun. 23, 2015 for U.S. Appl. No. 13/525,640. Third Party Submission Under 37 CFR 1.290 in U.S. Appl. No. 14/188,504 submitted May 11, 2015 and May 27, 2015 (43 pages). Naguib et al., "Fundamental Foaming Mechanisms Governing the Volume Expansion of Extruded Polypropylene Foams," Journal of Applied Polymer Science, vol. 91, pp. 2661-2668, 2004 (10 pages). Wang et al., "Extending PP\s Foamability Through Tailored Melt Strength and Crystallization Kinetics," paper 19 from the Conference Proceedings of the 8th International Conferences of Blowing Agents and Foaming Processes, May 16-17, 2006 in Munich, Germany Smithers Rapra Ltd, 2006 (14 pages).



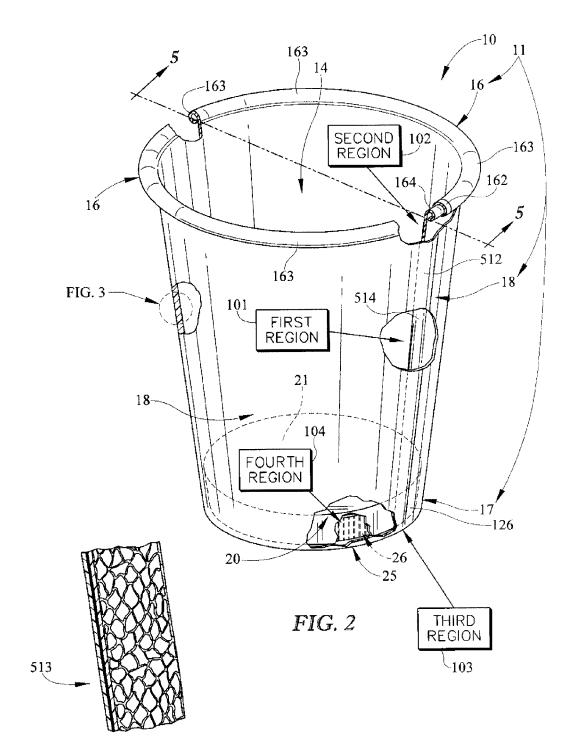
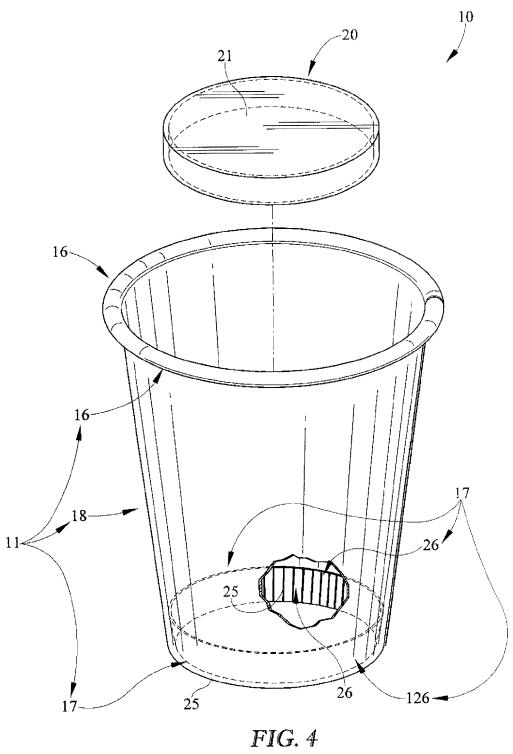


FIG. 3



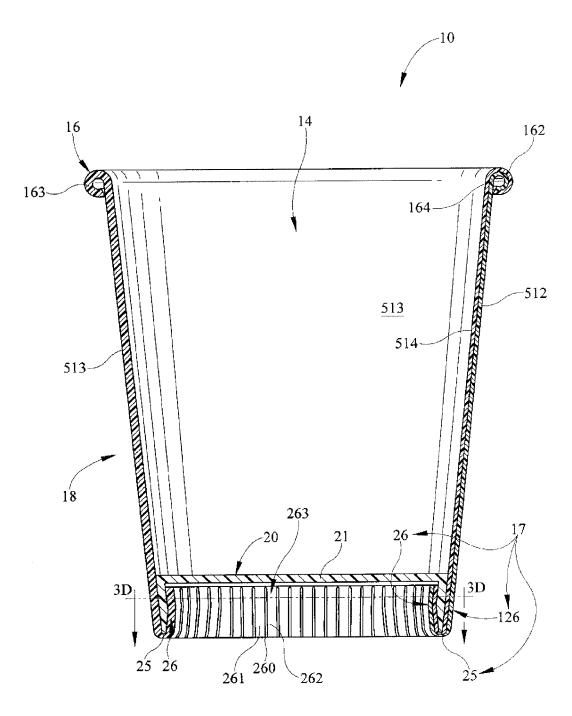
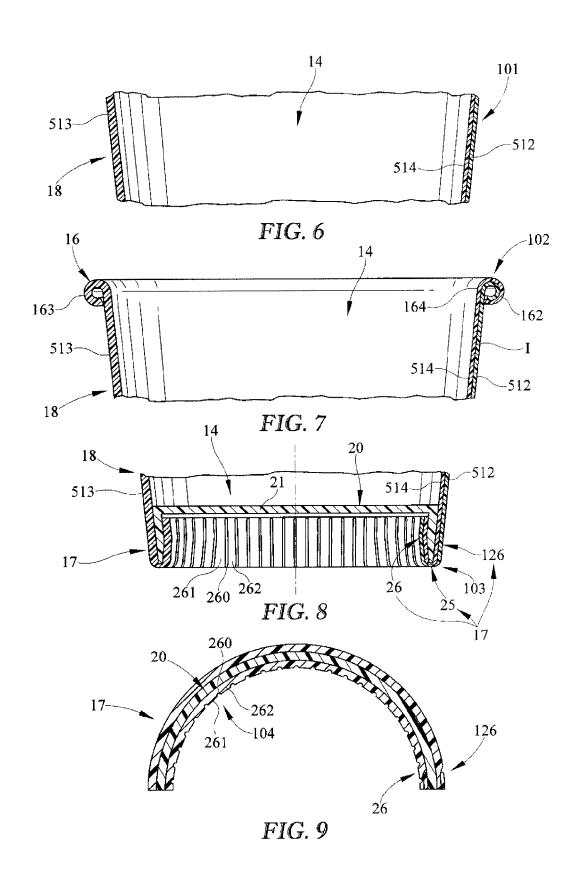


FIG. 5



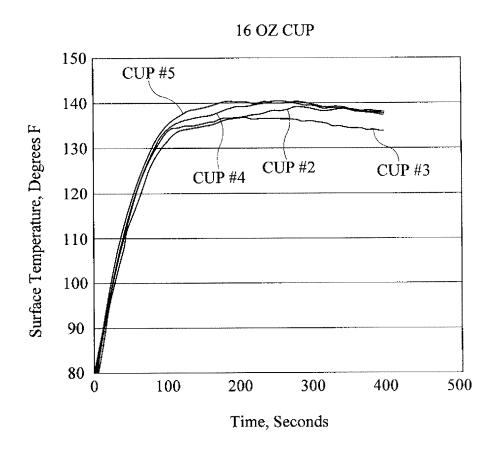


FIG. 10

## POLYMERIC MATERIAL FOR AN INSULATED CONTAINER

#### PRIORITY CLAIM

This application is a continuation of U.S. application Ser. No. 13/491,327, filed Jun. 7, 2012, which claims priority under 35 U.S.C. §119(e) to U.S. Provisional Application Ser. No. 61/529,632, filed Aug. 31, 2011 and U.S. Provisional Application Ser. No. 61/618,604, filed Mar. 30, 2012, each of which is expressly incorporated by reference herein.

#### BACKGROUND

The present disclosure relates to polymeric materials that 15 can be formed to produce a container, and in particular, polymeric materials that insulate. More particularly, the present disclosure relates to polymer-based formulations that can be formed to produce an insulated non-aromatic polymeric material.

#### **SUMMARY**

A polymeric material in accordance with the present disclosure includes a polymeric resin and cell-forming agents. In 25 illustrative embodiments, a blend of polymeric resins and cell-forming agents is extruded or otherwise formed to produce an insulated cellular non-aromatic polymeric material.

In illustrative embodiments, an insulative cellular non-aromatic polymeric material produced in accordance with the 30 present disclosure can be formed to produce an insulative cup or other product. Polypropylene resin is used to form the insulative cellular non-aromatic polymeric material in illustrative embodiments.

In illustrative embodiments, an insulative cellular non-aromatic polymeric material comprises a polypropylene base resin having a high melt strength, a polypropylene copolymer or homopolymer (or both), and cell-forming agents including at least one nucleating agent and a blowing agent such as carbon dioxide. In illustrative embodiments, the insulative 40 cellular non-aromatic polymeric material further comprises a slip agent. The polypropylene base resin has a broadly distribution

In illustrative embodiments, a polypropylene-based formulation in accordance with the present disclosure is heated and extruded in two stages to produce a tubular extrudate (in an extrusion process) that can be sliced to provide a strip of insulative cellular non-aromatic polymeric material. A blowing agent in the form of an inert gas is introduced into a molten serior in the first extrusion stage in illustrative embodiments.

In illustrative embodiments, an insulative cup is formed using the strip of insulative cellular non-aromatic polymeric material. The insulative cup includes a body having a sleeve-shaped side wall and a floor coupled to the body to cooperate 55 with the side wall to form an interior region for storing food, liquid, or any suitable product. The body also includes a rolled brim coupled to an upper end of the side wall and a floor mount coupled to a lower end of the side wall and to the floor.

The insulative cellular non-aromatic polymeric material is 60 configured in accordance with the present disclosure to provide means for enabling localized plastic deformation in at least one selected region of the body (e.g., the side wall, the rolled brim, the floor mount, and a floor-retaining flange included in the floor mount) to provide (1) a plastically 65 deformed first material segment having a first density in a first portion of the selected region of the body and (2) a second

2

material segment having a relatively lower second density in an adjacent second portion of the selected region of the body. In illustrative embodiments, the first material segment is thinner than the second material segment.

Additional features of the present disclosure will become apparent to those skilled in the art upon consideration of illustrative embodiments exemplifying the best mode of carrying out the disclosure as presently perceived.

#### BRIEF DESCRIPTIONS OF THE DRAWINGS

The detailed description particularly refers to the accompanying figures in which:

FIG. 1 is a diagrammatic and perspective view of a material-forming process in accordance with the present disclosure showing that the material-forming process includes, from left to right, a formulation of insulative cellular nonaromatic polymeric material being placed into a hopper that is fed into a first extrusion zone of a first extruder where heat and pressure are applied to form molten resin and showing that a blowing agent is injected into the molten resin to form an extrusion resin mixture that is fed into a second extrusion zone of a second extruder where the extrusion resin mixture exits and expands to form an extrudate which is slit to form a strip of insulative cellular non-aromatic polymeric material;

FIG. 2 is a perspective view of an insulative cup made from a strip of material including the insulative cellular non-aromatic polymeric material of FIG. 1 showing that the insulative cup includes a body and a floor and showing that four regions of the body have been broken away to reveal localized areas of plastic deformation that provide for increased density in those areas while maintaining a predetermined insulative characteristic in the body;

FIG. 3 is an enlarged sectional view of a portion of a side wall included in the body of the insulative cup of FIG. 2 showing that the side wall is made from a sheet that includes, from left to right, a skin including a film, an ink layer, and an adhesive layer, and the strip of insulative cellular non-aromatic polymeric material of FIG. 1;

FIG. 4 is an exploded assembly view of the insulative cup of FIG. 2 showing that the insulative cup includes, from top to bottom, the floor and the body including a rolled brim, the side wall, and a floor mount configured to interconnect the floor and the side wall as shown in FIG. 2;

FIG. 5 is a sectional view taken along line 5-5 of FIG. 2 showing that the side wall included in the body of the insulative cup includes a generally uniform thickness and that the floor is coupled to the floor mount included in the body;

FIGS. **6-9** are a series views showing first, second, third, and fourth regions of the insulative cup of FIG. **2** that each include localized plastic deformation;

FIG. 6 is a partial section view taken along line 5-5 of FIG. 2 showing the first region is in the side wall of the body;

FIG. 7 is a partial section view taken along line 5-5 of FIG. 2 showing the second region is in the rolled brim of the body;

FIG. 8 is a partial section view taken along line 5-5 of FIG. 2 showing the third region is in a connecting web included in the floor mount of the body;

FIG. 9 is a partial section view taken along line 5-5 of FIG. 2 showing the fourth region is in a web-support ring included in the floor mount of the body; and

FIG. 10 is a graph showing performance over time of insulative cups in accordance with the present disclosure undergoing temperature testing.

#### DETAILED DESCRIPTION

An insulative cellular non-aromatic polymeric material produced in accordance with the present disclosure can be

formed to produce an insulative cup 10 as suggested in FIGS. 2-9. As an example, the insulative cellular non-aromatic polymeric material comprises a polypropylene base resin having a high melt strength, a polypropylene copolymer or homopolymer (or both), and cell-forming agents including at least one 5 nucleating agent and a blowing agent such as carbon dioxide. As a further example, the insulative cellular non-aromatic polymeric material further comprises a slip agent. The polypropylene base resin has a broadly distributed unimodal (not bimodal) molecular weight distribution.

A material-forming process 100 uses a polypropylene-based formulation 121 in accordance with the present disclosure to produce a strip 82 of insulative cellular non-aromatic polymeric material as shown in FIG. 1. Formulation 121 is heated and extruded in two stages to produce a tubular extrudate 124 that can be slit to provide strip 82 of insulative cellular non-aromatic polymeric material as illustrated, for example, in FIG. 1. A blowing agent in the form of a liquified inert gas is introduced into a molten resin 122 in the first extrusion zone.

Insulative cellular non-aromatic polymeric material is used to form insulative cup 10. Insulative cup 10 includes a body 11 having a sleeve-shaped side wall 18 and a floor 20 as shown in FIGS. 2 and 4. Floor 20 is coupled to body 11 and cooperates with side wall 18 to form an interior region 14 25 therebetween for storing food, liquid, or any suitable product. Body 11 also includes a rolled brim 16 coupled to an upper end of side wall 18 and a floor mount 17 coupled to a lower end of side wall 18 and to floor 20 as shown in FIG. 5.

Insulative cellular non-aromatic polymeric material is configured in accordance with the present disclosure to provide means for enabling localized plastic deformation in at least one selected region of body 11 (e.g., side wall 18, rolled brim 16, floor mount 17, and a floor-retaining flange 26 included in floor mount 17) to provide (1) a plastically deformed first 35 material segment having a first density in a first portion of the selected region of body 11 and (2) a second material segment having a relatively lower second density in an adjacent second portion of the selected region of body 11 as suggested, for example, in FIGS. 2 and 6-9. In illustrative embodiments, the 40 first material segment is thinner than the second material segment.

One aspect of the present disclosure provides a formulation for manufacturing an insulative cellular non-aromatic polymeric material. As referred to herein, an insulative cellular 45 non-aromatic polymeric material refers to an extruded structure having cells formed therein and has desirable insulative properties at given thicknesses. Another aspect of the present disclosure provides a resin material for manufacturing an extruded structure of insulative cellular non-aromatic poly- 50 meric material. Still another aspect of the present disclosure provides an extrudate comprising an insulative cellular nonaromatic polymeric material. Yet another aspect of the present disclosure provides a structure of material formed from an insulative cellular non-aromatic polymeric material. A fur- 55 ther aspect of the present disclosure provides a container formed from an insulative cellular non-aromatic polymeric material.

In exemplary embodiments, a formulation includes at least one polymeric material. In one exemplary embodiment a 60 primary or base polymer comprises a high melt strength polypropylene that has long chain branching. Long chain branching occurs by the replacement of a substituent, e.g., a hydrogen atom, on a monomer subunit, by another covalently bonded chain of that polymer, or, in the case of a graft copolymer, by a chain of another type. For example, chain transfer reactions during polymerization could cause branching of the

4

polymer. Long chain branching is branching with side polymer chain lengths longer than the average critical entanglement distance of a linear polymer chain. Long chain branching is generally understood to include polymer chains with at least 20 carbon atoms depending on specific monomer structure used for polymerization. Another example of branching is by crosslinking of the polymer after polymerization is complete. Some long chain branch polymers are formed without crosslinking. Polymer chain branching can have a significant impact on material properties. Final selection of a polypropylene material may take into account the properties of the end material, the additional materials needed during formulation, as well as the conditions during the extrusion process. In exemplary embodiments high melt strength polypropylenes may be materials that can hold a gas (as discussed hereinbelow), produce desirable cell size, have desirable surface smoothness, and have an acceptable odor level (if any).

One illustrative example of a suitable polypropylene base resin is DAPLOY<sup>TM</sup> WB140 homopolymer (available from Borealis A/S), a high melt strength structural isomeric modified polypropylene homopolymer (melt strength=36, as tested per ISO 16790 which is incorporated by reference herein, melting temperature=325.4° F. (163° C.) using ISO 11357, which is incorporated by reference herein).

Borealis DAPLOY<sup>TM</sup> WB140 properties (as described in a Borealis product brochure):

	Property	Typical Value	Unit	Test Method
	Melt Flow Rate (230/2.16)	2.1	g/10 min	ISO 1133
	Flexural Modulus	1900	MPa	ISO 178
	Tensile Strength at Yield	40	MPa	ISO 527-2
	Elongation at Yield	6	%	ISO 527-2
	Tensile Modulus	2000	MPa	ISO 527-2
	Charpy impact strength, notched (+23° C.)	3.0	kJ/m <sup>2</sup>	ISO 179/1eA
	Charpy impact strength, notched (-20° C.)	1.0	kJ/m <sup>2</sup>	ISO 179/1eA
ı	Heat Deflection Temperature A (at 1.8 MPa load)	60	°C.	ISO 75-2 Method A
	Heat Deflection Temperature B (at 0.46 MPa load)	110	° C.	ISO 75-2 Method B

Other polypropylene polymers having suitable melt strength, branching, and melting temperature may also be used. Several base resins may be used and mixed together.

In certain exemplary embodiments, a secondary polymer may be used with the base polymer. The secondary polymer may be, for example, a polymer with sufficient crystallinity. In exemplary embodiments the secondary polymer may be at least one crystalline polypropylene homopolymer, an impact copolymer, mixtures thereof or the like. One illustrative example is a high crystalline polypropylene homopolymer, available as F020HC from Braskem. Another illustrative example is a polymer commercially available as PRO-FAX SC204<sup>™</sup> (available from LyndellBasell Industries Holdings, B.V.). Another illustrative example is Homo PP—INSPIRE 222, available from Braskem. In one aspect the polypropylene may have a high degree of crystallinity, i.e., the content of the crystalline phase exceeds 51% (as tested using differential scanning calorimetry) at 10° C./min cooling rate. In exemplary embodiments several different secondary polymers may be used and mixed together.

In exemplary embodiments, the secondary polymer may be or may include polyethylene. In exemplary embodiments, the secondary polymer may include low density polyethylene,

linear low density polyethylene, high density polyethylene, ethylene-vinyl acetate copolymers, ethylene-ethylacrylate copolymers, ethylene-acrylic acid copolymers, mixtures of at least two of the foregoing and the like. The use of non-polypropylene materials may affect recyclability, insulation, 5 microwavability, impact resistance, or other properties, as discussed further hereinbelow.

One or more nucleating agents are used to provide and control nucleation sites to promote formation of cells, bubbles, or voids in the molten resin during the extrusion 10 process. Nucleating agent means a chemical or physical material that provides sites for cells to form in a molten resin mixture. Nucleating agents may be physical agents or chemical agents. Suitable physical nucleating agents have desirable particle size, aspect ratio, and top-cut properties. Examples 15 include, but are not limited to, talc, CaCO<sub>3</sub>, mica, and mixtures of at least two of the foregoing. The nucleating agent may be blended with the polymer resin formulation that is introduced into the hopper. Alternatively, the nucleating agent may be added to the molten resin mixture in the extruder. 20 When the chemical reaction temperature is reached the nucleating agent acts to enable formation of bubbles that create cells in the molten resin. An illustrative example of a chemical blowing agent is citric acid or a citric acid-based material. After decomposition, the chemical blowing agent forms 25 small gas cells which further serve as nucleation sites for larger cell growth from a physical or other types of blowing agents. One representative example is Hydrocerol<sup>TM</sup> CF-40E™ (available from Clariant Corporation), which contains citric acid and a crystal nucleating agent. In illustrative 30 embodiments one or more catalysts or other reactants may be added to accelerate or facilitate the formation of cells.

In certain exemplary embodiments, one or more blowing agents may be incorporated. Blowing agent means a physical or a chemical material (or combination of materials) that acts 35 to expand nucleation sites. Nucleating agents and blowing agents may work together. The blowing agent acts to reduce density by forming cells in the molten resin. The blowing agent may be added to the molten resin mixture in the extruder. Representative examples of physical blowing 40 agents include, but are not limited to, carbon dioxide, nitrogen, helium, argon, air, pentane, butane, or other alkane mixtures of the foregoing and the like. In certain exemplary embodiments, a processing aid may be employed that enhances the solubility of the physical blowing agent. Alter- 45 natively, the physical blowing agent may be a hydrofluorocarbon, such as 1.1.1.2-tetrafluoroethane, also known as R134a, or other haloalkane refrigerant. Selection of the blowing agent may be made to take environmental impact into consideration.

In exemplary embodiments, physical blowing agents are typically gases that are introduced as liquids under pressure into the molten resin via a port in the extruder as suggested in FIG. 1. As the molten resin passes through the extruder and the die head, the pressure drops causing the physical blowing 55 agent to change phase from a liquid to a gas, thereby creating cells in the extruded resin. Excess gas blows off after extrusion with the remaining gas being trapped in the cells in the extrudate.

Chemical blowing agents are materials that degrade or 60 react to produce a gas. Chemical blowing agents may be endothermic or exothermic. Chemical blowing agents typically degrade at a certain temperature to decompose and release gas. In one aspect the chemical blowing agent may be one or more materials selected from the group consisting of 65 azodicarbonamide; azodiisobutyro-nitrile; benzenesulfonhydrazide; 4,4-oxybenzene sulfonylsemicarbazide; p-toluene

6

sulfonyl semi-carbazide; barium azodicarboxylate; N,N'dimethyl-N,N'-dinitrosoterephthalamide; trihydrazino triazine; methane; ethane; propane; n-butane; isobutane; n-pentane: isopentane; neopentane; methyl perfluoromethane; ethyl fluoride; 1,1-difluoroethane; 1,1,1trifluoroethane; 1,1,1,2-tetrafluoro-ethane; pentafluoroethane; perfluoroethane; 2,2-difluoropropane; 1,1,1-trifluoropropane; perfluoropropane; perfluorobutane; perfluorocyclobutane; methyl chloride; methylene chloride; ethyl chloride; 1,1,1-trichloroethane; 1,1-dichloro-1-fluoroethane; 1-chloro-1,1-difluoroethane; 1,1-dichloro-2,2,2-trifluoroethane; 1-chloro-1,2,2,2-tetrafluoroethane; trichloromonofluoromethane; dichlorodifluoromethane; trichlorotrifluoroethane; dichlorotetrafluoroethane; chloroheptafluoropropane; dichlorohexafluoropropane; methanol; ethanol; n-propanol; isopropanol; sodium bicarbonate; sodium carbonate; ammonium bicarbonate; ammonium carbonate; ammonium nitrite; N,N'-dimethyl-N,N'-dinitrosoterephthalamide; N,N'-dinitrosopentamethylene tetramine; azobisisobutylonitrile; azocyclohexylnitrile; azodiaminobenzene; benzene sulfonyl hydrazide; toluene sulfonyl hydrazide; p,p'-oxybis(benzene sulfonyl hydrazide); diphenyl sulfone-3,3'-disulfonyl hydrazide; calcium azide; 4,4'diphenyl disulfonyl azide; and p-toluene sulfonyl azide.

In one aspect of the present disclosure, where a chemical blowing agent is used, the chemical blowing agent may be introduced into the resin formulation that is added to the hopper.

In one aspect of the present disclosure, the blowing agent may be a decomposable material that forms a gas upon decomposition. A representative example of such a material is citric acid or a citric-acid based material. In one exemplary aspect of the present disclosure it may be possible to use a mixture of physical and chemical blowing agents.

In one aspect of the present disclosure, at least one slip agent may be incorporated into the resin mixture to aid in increasing production rates. Slip agent (also known as a process aid) is a term used to describe a general class of materials which are added to a resin mixture and provide surface lubrication to the polymer during and after conversion. Slip agents may also reduce or eliminate die drool. Representative examples of slip agent materials include amides of fats or fatty acids, such as, but not limited to, erucamide and oleamide. In one exemplary aspect, amides from oleyl (single unsaturated C-18) through erucyl (C-22 single unsaturated) may be used. Other representative examples of slip agent materials include low molecular weight amides and fluoroelastomers. Combinations of two or more slip agents can be used. Slip agents may be provided in a master batch pellet form and blended with the resin formulation.

One or more additional components and additives optionally may be incorporated, such as, but not limited to, impact modifiers, colorants (such as, but not limited to, titanium dioxide), and compound regrind.

The polymer resins may be blended with any additional desired components and melted to form a resin formulation mixture

In addition to surface topography and morphology, another factor that was found to be beneficial to obtain a high quality insulative cup free of creases was the anisotropy of the insulative cellular non-aromatic polymeric strip. Aspect ratio is the ratio of the major axis to the minor axis of the cell. As confirmed by microscopy, in one exemplary embodiment the average cell dimensions in a machine direction 67 (machine or along the web direction) of an extruded strip 82 of insulative cellular non-aromatic polymeric material was about 0.0362 inches (0.92 mm) in width by about 0.0106 inches

(0.27 mm) in height. As a result, a machine direction cell size aspect ratio is about 3.5. The average cell dimensions in a cross direction (cross-web or transverse direction) was about 0.0205 inches (0.52 mm) in width and about 0.0106 inches (0.27 mm) in height. As a result, a cross-direction aspect ratio is 1.94. In one exemplary embodiment, it was found that for the strip to withstand compressive force during cup forming, one desirable average aspect ratio of the cells was between about 1.0 and about 3.0. In one exemplary embodiment one desirable average aspect ratio of the cells was between about 10 1.0 and about 2.0.

The ratio of machine direction to cross direction cell length is used as a measure of anisotropy of the extruded strip. In exemplary embodiments, a strip of insulative cellular nonaromatic polymeric material may be bi-axially oriented, with 15 a coefficient of anisotropy ranging between about 1.5 and about 3. In one exemplary embodiment, the coefficient of anisotropy was about 1.8.

If the circumference of the cup is aligned with machine direction 67 of extruded strip 82 with a cell aspect ratio 20 exceeding about 3.0, deep creases with depth exceeding about 200 microns are typically formed on inside surface of the cup making it unusable. Unexpectedly, it was found, in one exemplary embodiment, that if the circumference of the cup was aligned in the cross direction of extruded strip 82, which can 25 be characterized by cell aspect ratio below about 2.0, no deep creases were formed inside of the cup, indicating that the cross direction of extruded strip 82 was more resistant to compression forces during cup formation.

One possible reason for greater compressibility of an 30 extruded strip with cells having aspect ratio below about 2.0 in the direction of cup circumference, such as in the cross direction, could be due to lower stress concentration for cells with a larger radius. Another possible reason may be that the higher aspect ratio of cells might mean a higher slenderness 35 ratio of the cell wall, which is inversely proportional to buckling strength. Folding of the strip into wrinkles in the compression mode could be approximated as buckling of cell walls. For cell walls with longer length, the slenderness ratio (length to diameter) may be higher. Yet another possible fac- 40 tor in relieving compression stress might be a more favorable polymer chain packing in cell walls in the cross direction allowing polymer chain re-arrangements under compression force. Polymer chains are expected to be preferably oriented and more tightly packed in machine direction 67.

In exemplary embodiments, the combination of alignment of the formed cup circumference along the direction of the extruded strip where cell aspect ratio is below about 2.0. As a result, the surface of extruded strip with crystal domain size below about 100 angstroms facing inside the cup may provide 50 favorable results of achieving a desirable surface topography with imperfections less than about 5 microns deep.

In one aspect of the present disclosure, the polypropylene resin (either the base or the combined base and secondary about 0.19 g/cm<sup>3</sup>. In one exemplary embodiment, the density may be in a range of about 0.05 g/cm<sup>3</sup> to about 0.19 g/cm<sup>3</sup>. In one exemplary embodiment, the density may be in a range of about 0.1 g/cm<sup>3</sup> to about 0.185 g/cm<sup>3</sup>.

In an alternative exemplary embodiment, instead of 60 polypropylene as the primary polymer, a polylactic acid material may be used, such as, but not limited to, a polylactic acid material derived from a food-based material, for example, corn starch. In one exemplary embodiment, polyethylene may be used as the primary polymer.

In one exemplary aspect of the present disclosure, one formulation for a material useful in the formation of an insu-

lative cellular non-aromatic polymeric material includes the following: at least one primary resin comprising a high melt strength long chain branched polypropylene, at least one secondary resin comprising a high crystalline polypropylene homopolymer or an impact copolymer, at least one nucleating agent, at least one blowing agent, and at least one slip agent. Optionally, a colorant may be incorporated.

The formulation may be introduced into an extruder via a hopper, such as that shown in FIG. 1. During the extrusion process the formulation is heated and melted to form a molten resin mixture. In exemplary embodiments, at least one physical blowing agent is introduced into the molten resin mixture via one or more ports in the extruder. The molten resin mixture and gas is then extruded through a die.

In another exemplary embodiment, the formulation may contain both at least one chemical blowing agent and at least one physical blowing agent.

Cups or other containers or structures may be formed from the sheet according to conventional apparatus and methods.

For the purposes of non-limiting illustration only, formation of a cup from an exemplary embodiment of a material disclosed herein will be described; however, the container may be in any of a variety of possible shapes or structures or for a variety of applications, such as, but not limited to, a conventional beverage cup, storage container, bottle, or the like. For the purpose of nonlimiting illustration only, a liquid beverage will be used as the material which can be contained by the container; however, the container may hold liquids, solids, gels, combinations thereof, or other material.

A material-forming process 100 is shown, for example, in FIG. 1. Material-forming process 100 extrudes a non-aromatic polymeric material into a sheet or strip of insulative cellular non-aromatic polymeric material 82 as suggested in FIG. 1. As an example, material-forming process 100 uses a tandem-extrusion technique in which a first extruder 111 and a second extruder 112 cooperate to extrude strip of insulative cellular non-aromatic polymeric material 82.

As shown in FIG. 1, a formulation 121 of insulative cellular non-aromatic polymeric material 82 is loaded into a hopper 113 coupled to first extruder 111. The formulation 121 may be in pellet, granular flake, powder, or other suitable form. Formulation 121 of insulative cellular non-aromatic polymeric material is moved from hopper 113 by a screw 114 included in first extruder 111. Formulation 121 is transformed into a molten resin 122 in a first extrusion zone of first extruder 111 by application of heat 105 and pressure from screw 114 as suggested in FIG. 1. In exemplary embodiments a physical blowing agent 115 may be introduced and mixed into molten resin 122 after molten resin 122 is established. In exemplary embodiments, as discussed further herein, the physical blowing agent may be a gas introduced as a pressurized liquid via a port 115A and mixed with molten resin 122 to form a molten extrusion resin mixture 123, as shown in FIG. 1.

Extrusion resin mixture 123 is conveyed by screw 114 into resin) may have a density in a range of about 0.01 g/cm<sup>3</sup> to 55 a second extrusion zone included in second extruder 112 as shown in FIG. 1. There, extrusion resin mixture 123 is further processed by second extruder 112 before being expelled through an extrusion die 116 coupled to an end of second extruder 112 to form an extrudate 124. As extrusion resin mixture 123 passes through extrusion die 116, gas 115 comes out of solution in extrusion resin mixture 103 and begins to form cells and expand so that extrudate 124 is established. As an exemplary embodiment shown in FIG. 1 the extrudate 124 may be formed by an annular extrusion die 116 to form a tubular extrudate. A slitter 117 then cuts extrudate 124 to establish a sheet or strip 82 of insulative cellular non-aromatic polymeric material as shown in FIG. 1.

Extrudate means the material that exits an extrusion die. The extrudate material may be in a form such as, but not limited to, a sheet, strip, tube, thread, pellet, granule or other structure that is the result of extrusion of a polymer-based formulation as described herein through an extruder die. For 5 the purposes of illustration only, a sheet will be referred to as a representative extrudate structure that may be formed, but is intended to include the structures discussed herein. The extrudate may be further formed into any of a variety of final products, such as, but not limited to, cups, containers, trays, 10 wraps, wound rolls of strips of insulative cellular non-aromatic polymeric material, or the like.

As an example, strip 82 of insulative cellular non-aromatic polymeric material is wound to form a roll of insulative cellular non-aromatic polymeric material and stored for later 15 use. However, it is within the scope of the present disclosure for strip 82 of insulative cellular non-aromatic polymeric material to be used in-line with the cup-forming process. In one illustrative example, strip 82 of insulative cellular nonaromatic polymeric material is laminated with a skin having 20 a film and an ink layer printed on the film to provide high-

quality graphics.

An insulative cup 10 is formed using a strip 82 of insulative cellular non-aromatic polymeric material as shown in FIGS. 2 and 3. Insulative cup 10 includes, for example, a body 11 25 having a sleeve-shaped side wall 18 and a floor 20 coupled to body 11 to cooperate with the side wall 18 to form an interior region 14 for storing food, liquid, or any suitable product as shown in FIG. 2. Body 11 also includes a rolled brim 16 coupled to an upper end of side wall 18 and a floor mount 17 30 coupled to a lower end of side wall 18 and to the floor 20 as illustrated in FIGS. 2 and 7.

Body 11 is formed from a strip 82 of insulative cellular non-aromatic polymeric material as disclosed herein. In accordance with the present disclosure, strip 82 of insulative 35 cellular non-aromatic polymeric material is configured through application of pressure and heat (though in exemplary embodiments configuration may be without application of heat) to provide means for enabling localized plastic deformation in at least one selected region of body 11 to provide a 40 plastically deformed first sheet segment having a first density located in a first portion of the selected region of body 11 and a second sheet segment having a second density lower than the first density located in an adjacent second portion of the selected region of body 11 without fracturing the sheet of 45 insulative cellular non-aromatic polymeric material so that a predetermined insulative characteristic is maintained in body

A first 101 of the selected regions of body 11 in which localized plastic deformation is enabled by the insulative 50 cellular non-aromatic polymeric material is in sleeve-shaped side wall 18 as suggested in FIGS. 2, 5, and 6. Sleeve-shaped side wall 18 includes an upright inner tab 514, an upright outer tab **512**, and an upright fence **513** as suggested in FIGS. 2, 5, and 6. Upright inner tab 514 is arranged to extend 55 upwardly from floor 20 and configured to provide the first sheet segment having the first density in the first 101 of the selected regions of body 11. Upright outer tab 512 is arranged to extend upwardly from floor 20 and to mate with upright inner tab 514 along an interface I therebetween as suggested 60 in FIG. 6. Upright fence 513 is arranged to interconnect upright inner and outer tabs 514, 512 and surround interior region 14. Upright fence 513 is configured to provide the second sheet segment having the second density in the first 101 of the selected regions of body 11 and cooperate with 65 upright inner and outer tabs 514, 512 to form sleeve-shaped side wall 18 as suggested in FIGS. 2-5.

10

A second 102 of the selected regions of body 11 in which localized plastic deformation is enabled by the sheet of insulative cellular non-aromatic polymeric material is in rolled brim 16 included in body 11 as suggested in FIGS. 2, 4, 5, and 7. Rolled brim 16 is coupled to an upper end of sleeve-shaped side wall 18 to lie in spaced-apart relation to floor 20 and to frame an opening into interior region 14. Rolled brim 16 includes an inner rolled tab 164, an outer rolled tab 162, and a rolled lip 163 as suggested in FIGS. 2, 4, 5, and 7. Inner rolled tab 164 is configured to provide the first sheet segment in the second 102 of the selected regions of body 11. Inner rolled tab 164 is coupled to an upper end of upright outer tab 512 included in sleeve-shaped side wall 18. Outer rolled tab 162 is coupled to an upper end of upright inner tab 514 included in sleeve-shaped side wall 18 and to an outwardly facing exterior surface of inner rolled tab 164. Rolled lip 163 is arranged to interconnect oppositely facing side edges of each of inner and outer rolled tabs 164, 162. Rolled lip 163 is configured to provide the second sheet segment having the second density in the second 102 of the selected region of body 11 and cooperate with inner and outer rolled tabs 164, 162 to form rolled brim 16 as suggested in FIG. 2.

A third 103 of the selected regions of body 11 in which localized plastic deformation is enabled by the sheet of insulative cellular non-aromatic polymeric material is in a floor mount included in body 11 as suggested in FIGS. 2, 5, and 8. Floor mount 17 is coupled to a lower end of sleeve-shaped side wall 18 to lie in spaced-apart relation to rolled brim 16 and to floor 20 to support floor 20 in a stationary position relative to sleeve-shaped side wall 18 to form interior region 14. Floor mount 17 includes a web-support ring 126, a floorretaining flange 26, and a web 25. Web-support ring 126 is coupled to the lower end of sleeve-shaped side wall 18 and configured to provide the second sheet segment having the second density in the third 103 of the selected regions of body 11. Floor-retaining flange 26 is coupled to floor 20 and arranged to be surrounded by web-support ring 126. Web 25 is arranged to interconnect floor-retaining flange 26 and websupport ring 126. Web 25 is configured to provide the first sheet segment having the first density in the third 103 of the selected regions of body 11.

A fourth 104 of the selected regions of body 11 in which localized plastic deformation is enabled by the sheet of insulative cellular non-aromatic polymeric material is in floorretaining flange of floor mount 17 as suggested in FIGS. 2, 5, and 9. Floor-retaining flange 26 includes an alternating series of upright thick and thin staves arranged in side-to-side relation to extend upwardly from web 25 toward interior region 14 bounded by sleeve-shaped side wall 18 and floor 20. A first 261 of the upright thick staves is configured to include a right side edge extending upwardly from web 25 toward interior region 14. A second 262 of the upright thick staves is configured to include a left side edge arranged to extend upwardly from web 25 toward interior region 14 and lie in spaced-apart confronting relation to right side edge of the first 261 of the upright thick staves. A first 260 of the upright thin staves is arranged to interconnect left side edge of the first 261 of the upright thick staves and right side edge of the second 262 of the upright thick staves and to cooperate with left and right side edges to define therebetween a vertical channel 263 opening inwardly into a lower interior region bounded by floor-retaining flange 26 and a horizontal platform 21 included in floor 20 and located above floor-retaining flange 26. The first 260 of the upright thin staves is configured to provide the first sheet segment in the fourth 104 of the selected regions of body 11. The first 261 of the upright thick

staves is configured to provide the second sheet segment in the fourth 104 of the selected regions of the body 11.

The compressibility of the insulative cellular non-aromatic polymeric material used to produce insulative cup 10 allows the insulative cellular non-aromatic polymeric material to be 5 prepared for the mechanical assembly of insulative cup 10. without limitations experienced by other non-aromatic polymeric materials. The cellular nature of the material provides insulative characteristics as discussed below, while susceptibility to plastic deformation permits yielding of the material without fracture. The plastic deformation experienced when the insulative cellular non-aromatic polymeric material is subjected to a pressure load is used to form a permanent set in the insulative cellular non-aromatic polymeric material after 15 the pressure load has been removed. In some locations, the locations of permanent set are positioned to provide controlled gathering of the sheet of insulative cellular non-aromatic polymeric material.

The plastic deformation may also be used to create fold 20 lines in the sheet to control deformation of the sheet when being worked during the assembly process. When deformation is present, the absence of material in the voids formed by the deformation provides relief to allow the material to be easily folded at the locations of deformation.

A potential unexpected feature of the sheet of insulative cellular non-aromatic polymeric material formed as described herein is the high insulation value obtained at a given thickness. See, for example, Examples 1 and 2 below.

A potential feature of a cup formed of insulative cellular 30 non-aromatic polymeric material according to exemplary embodiments of the present disclosure is that the cup has low material loss. Furthermore, the material of the present disclosure may have markedly low off-gassing when subjected to heat from a conventional kitchen-type microwave oven for 35 periods of time up to several minutes.

Another potential feature of a cup formed of the insulative cellular non-aromatic polymeric material according to the present disclosure is that the cup can be placed in and go through a conventional residential or commercial dishwasher 40 cleaning cycle (top rack) without noticeable structural or material breakdown or adverse affect on material properties. This is in comparison to beaded expanded polystyrene cups or containers which can break down under similar cleaning processes. Accordingly, a cup made according to one aspect of 45 the present disclosure can be cleaned and reused.

Another potential feature of an article formed of the insulative cellular non-aromatic polymeric material according to various aspects of the present disclosure is that the article can be recycled. Recyclable means that a material can be added 50 (such as regrind) back into an extrusion or other formation process without segregation of components of the material, i.e., an article formed of the material does not have to be manipulated to remove one or more materials or components prior to re-entering the extrusion process. For example, a cup 55 having a printed film layer laminated to the exterior of the cup may be recyclable if one does not need to separate out the film layer prior to the cup being ground into particles. In contrast, a paper-wrapped expanded polystyrene cup may not be recyclable because the polystyrene material could not practicably 60 be used as material in forming an expanded polystyrene cup, even though the cup material may possibly be formed into another product. As a further example, a cup formed from a non-expanded polystyrene material having a layer of nonstyrene printed film adhered thereto may be considered non- 65 recyclable because it would require the segregation of the polystyrene cup material from the non-styrene film layer,

12

which would not be desirable to introduce as part of the regrind into the extrusion process.

Recyclability of articles formed from the insulative cellular non-aromatic polymeric material of the present disclosure minimizes the amount of disposable waste created. In comparison, beaded expanded polystyrene cups break up into beads and thus ordinarily cannot easily be reused in a manufacturing process with the same material from which the article was formed. And, paper cups that typically have an extrusion coated plastic layer or a plastic lamination for liquid resistance ordinarily cannot be recycled because the different materials (paper, adhesive, film, plastic) normally cannot be practicably separated in commercial recycling operations.

A potential feature of a cup or other article formed of material according to one aspect (a non-laminate process) of the present disclosure is that the outside (or inside or both) wall surface of the insulative cellular non-aromatic polypropylene sheet (prior to being formed into a cup, or during cup formation, depending on the manufacturing process employed) can accept printing of high-resolution graphics. Conventional beaded expanded polystyrene cups have a surface which typically is not smooth enough to accept printing other than low-resolution graphics. Similarly, known uncoated paper cups also typically do not have a smooth enough surface for such high-resolution graphics. Paper cups can be coated to have the desired surface finish and can achieve high resolution. Paper has difficulty reaching insulation levels and requires a designed air gap incorporated into or associated with the cup to achieve insulation, such as a sleeve slid onto and over a portion of the cup. Accordingly, solutions have been to use low-resolution printing, laminate to the outside wall a film which has been printed, or to have a printed sleeve (either bonded or removable) inserted over the outside wall or coat the paper to accept high resolution graphics.

A potential feature of a cup formed of the insulative cellular non-aromatic polymeric material according to one aspect of the present disclosure is that it possesses unexpected strength as measured by rigidity. Rigidity is a measurement done at room temperature and at an elevated temperature (e.g., by filling the cup with a hot liquid) and measuring the rigidity of the material. The strength of the cup material is important to reduce the potential for the cup being deformed by a user and the lid popping off or the lid or sidewall seal leaking.

A potential feature of a cup formed of the insulative cellular non-aromatic polymeric material according to the present disclosure is that the sleeve is resistant to puncture, such as by a straw, fork, spoon, finger nail, or the like, as measured by standard impact testing, as described hereinbelow. Test materials demonstrated substantially higher impact resistance when compared to a beaded expanded polystyrene cup. Accordingly, a cup formed as described herein can reduce the likelihood of puncture and leakage of hot liquid onto a user.

A feature of a cup with a compressed brim and seam formed of the material according to one aspect as described herein is that a greater number of such cups can be nested in a given sleeve length because the seam is thinner and the side wall angle can be minimized (i.e., more approaching 90° with respect to the cup bottom) while providing a sufficient air gap to permit easy de-nesting. Conventionally seam-formed cups having a seam substantially thicker than the side wall requires a greater side wall angle (and air gap) to allow for de-nesting, resulting in fewer cups being able to be nested in a given sleeve length.

A feature of a cup formed of the material according to one aspect of the present disclosure is that the brim may have a cross-section profile of less than about 0.170 inches (4.318)

mm) which may be due to localized cell deformation and compression. Such a small profile is more aesthetically pleasing than a larger profile.

A feature of a cup formed of the material according to one aspect of the present disclosure is that the rolled brim diameter can be the same for cups of different volumes, enabling one lid size to be used for different cup sizes, assuming the cup rims outside diameters are the same. As a result, the number of different size lids in inventory and at the point of use may be reduced.

The material formulation may have properties that allow the sheet to be compressed without fracturing.

The insulative cellular non-aromatic polymeric material of the present disclosure may be formed into a strip which can be  $_{15}$ wrapped around other structures. For example, a strip of the material according to one aspect of the present disclosure that can be used as a wrapping material may be formed and wrapped around a pipe, conduit, or other structure to provide improved insulation. The sheet or strip may have a layer of 20 adhesive, such as a pressure sensitive adhesive, applied to one or both faces. The strip may be wound onto a roll. Optionally, the strip may have a release liner associated therewith to make unwinding the strip from the roll easier. The polymer formulation may be adapted to provide the requisite flexibility to 25 form a wrap or windable strip, for example, by using one or more polypropylene or other polyolefin materials that have sufficient flexibility to enable the extruded sheet to be flexible enough to be wound onto a roll. The insulative cellular nonaromatic polymeric material may be formed into a sleeve that can be inserted over a cup to provide additional insulation.

In exemplary embodiments sheets formed from the insulative cellular non-aromatic polymeric material of the present disclosure may be cut at the die or be flaked and used as a bulk insulator.

The formulation and insulative cellular non-aromatic polymeric material of the present disclosure satisfies a long-felt need for a material that can be formed into an article, such as a cup, that includes many if not all of the features of insulative 40 performance, ready for recyclability, puncture resistance, frangibility resistance, microwavability and other features as discussed herein. Others have failed to provide a material that achieves combinations of these features as reflected in the appended claims. This failure is a result of the features being associated with competitive design choices. As an example, others have created materials and structures therefrom that based on design choices are insulated but suffer from poor puncture resistance, inability to effectively be recyclable, and lack microwavability. In comparison, the formulations and 50 materials disclosed herein overcome the failures of others by using an insulative cellular non-aromatic polymeric material. Reference is hereby made to U.S. application Ser. No. 13/491, 007 filed Jun. 7, 2012 and entitled INSULATED CON-TAINER for disclosure relating to articles, such as cups, 55 formed from such insulative cellular non-aromatic polymeric materials, which application is hereby incorporated in its entirety herein.

#### **EXAMPLES**

The following examples are set forth for purposes of illustration only. Parts and percentages appearing in such examples are by weight unless otherwise stipulated. All ASTM, ISO and other standard test method cited or referred 65 to in this disclosure are incorporated by reference in their entirety.

14

#### Example 1

#### Formulation and Extrusion

DAPLOY<sup>TM</sup> WB140 polypropylene homopolymer (available from Borealis A/S) was used as the polypropylene base resin. F020HC, available from Braskem, a polypropylene homopolymer resin, was used as the secondary resin. The two resins were blended with: Hydrocerol<sup>TM</sup> CF-40E<sup>TM</sup> as a primary nucleation agent, talc as a secondary nucleation agent, CO<sub>2</sub> as a blowing agent, a slip agent, and titanium dioxide as a colorant. Percentages were:

79.9% Primary resin: high melt strength polypropylene Borealis WB140 HMS 15% Secondary resin: F020HC (Braskem)

0.1% Primary nucleating agent: Clariant Hyrocerol CF-40F<sup>TM</sup>

2% Secondary nucleating agent: Talc

1% Colorant: TiO<sub>2</sub> PE (alternatively, PP can be used)

2% Slip agent: Ampacet<sup>TM</sup> 102823 LLDPE (linear low-density polyethylene), available from Ampacet Corporation

The formulation was added to an extruder hopper. The extruder heated the formulation to form a molten resin mixture. To this mixture was added

1.1 lbs/hr CO<sub>2</sub>

0.7 lbs/hr R134a

The carbon dioxide with R134a was injected into the resin blend to expand the resin and reduce density. The mixture thus formed was extruded through a die head into a sheet. The sheet was then cut and formed into a cup.

#### Example 1

#### Test Results

The test results of the material formed according to Example 1 showed the material had a density of about 0.1902 g/cm<sup>3</sup> and a nominal sheet gauge of about 0.089 inches (2.2606 mm).

Microwavability

Containers produced using this material filled with 12 ounces of room temperature water were heated in a FISO Microwave Station (1200 Watts) microwave oven for 2.5 min without burning or scorching or other visible effect on the cup. In comparison, paper cups heated in the same microwave oven scorched or burned in less than 90 seconds.

Rigidity

Test Method

Samples were at  $73^{\circ}$  F.  $(22.8^{\circ}$  C.) and 50% relative humidity. The Cup Stiffness/Rigidity test was conducted with a horizontal force gauge containing a load cell to measure the resisting force of the cup when exposed to the following test conditions: (a) The test location on the cup was  $\frac{1}{3}$  down from the rim of the cup; (b) testing travel distance is 0.25 inches (6.35 mm); and (c) testing travel time was 10 seconds.

Test Results With an average wall thickness of about 0.064 inches (1.6256 mm), average density of about 0.1776 g/cm<sup>3</sup>, and average cup weight of about 9.86 g, the rigidity of the material

TABLE 1-continued Rigidity Test Results

16

	w in Tables	t 9.86 g, the rigidity 1-2.	or the materi	5			High Range Low Range	0.324 0.238
	T	ABLE 1		_	_		lidded/filled 200° F.	
	Rigidit	ty Test Results		_	_		Rigidities (kg-F)	
		unlidded/unfilled		10	Cup#	Seam	90° from Seam	Average
		Rigidities (kg-F)			16 17	0.346 0.386	0.354 0.422	0.350 0.404
Cup#	Seam	90° from Seam	Average		17 18 19	0.358 0.338	0.364 0.374	0.361 0.356
1 2	0.64 0.646	0.654 0.672	0.647 0.659	15	20	0.304	0.272 STD DEV	0.288 0.352 0.042
3 4 5	0.632 0.562 0.652	0.642 0.608 0.596	0.637 0.585 0.624				3 sigma High Range Low Range	0.125 0.476 0.227
		STD DEV	0.630 0.028	20 —				0.227
		3 sigma High Range	0.085 0.716	20		1	ınlidded/filled ice water	
		Low Range	0.545				Rigidities (kg-F)	
		lidded/unfilled			Cup#	Seam	$90^{\circ}$ from Seam	Averag
		Rigidities (kg-F)		25	21 22	0.796 0.818	0.730 0.826	0.763 0.822
Cup#	Seam	90° from Seam	Average	_	23 24	0.894 0.776	0.760 0.844	0.827 0.810
6 7	0.89 0.954	0.83 0.904	0.860 0.929	•	25	0.804	0.714	0.759 0.796
8 9 10	0.846 0.732 0.87	0.808 0.826 0.792	0.827 0.779 0.831	30			STD DEV 3 sigma High Range	0.033 0.098 0.894
10	0.87	STD DEV	0.845 0.055	_			Low Range	0.698
		3 sigma High Range	0.165 1.011	35	_		lidded/filled ice water	
		Low Range	0.680	_			Rigidities (kg-F)	
		unlidded/filled 200° F.			Cup#	Seam	90° from Seam	Averag
		Rigidities (kg-F)			26	1.044	0.892	0.968
Cup#	Seam	90° from Seam	Average	40 _	27 28	1.146 0.988	1.018 1.054	1.082 1.021
11 12 13	0.274 0.278 0.264	0.290 0.326 0.274	0.282 0.302 0.269		29 30	1.012 0.826	1.106 1.058	1.059 0.942 1.014
14 15	0.300 0.252	0.274 0.270 0.280	0.285 0.266	45			STD DEV 3 sigma	0.059 0.177
		STD DEV 3 sigma	0.281 0.014 0.043				High Range Low Range	1.192 0.837

TABLE 2

	Summary of Rigidity Test Results							
	Unfilled (kilogram	U	Hot Fill 200	° F. Kg-F	Ice Water F		Wall Thickness	Density
	Unlidded	Lidded	Unlidded	Lidded	Unlidded	Lidded	Inches	g/cc
Test material	0.630	0.845	0.281	0.352	0.796	1.014	0.064	0.1776

### In sulation

Test Method

A typical industrial cup insulation test method as follows was used:

Attach the (cup exterior) surface temperature thermocouple to cup with glue.

Tape attached thermocouple to cup with cellophane tape so that the thermocouple is in the middle of the cup opposite the seam.

Heat water or other aqueous liquid to near boiling, such as in a microwave.

Continually stir the hot liquid with a bulb thermometer while observing the liquid temperature.

Record thermocouple temperature.

When the liquid gets to  $200^{\circ}$  F. pour into cup to near full. 20 Place lid on cup.

Record surface temperature for a minimum of 5 minutes. Material thickness was about 0.089 inches (2.2606 mm). The density was about 0.1902 g/cm<sup>3</sup>.

Test Results

A cup formed from the formulation noted above was used having a density of about  $0.190~\text{g/cm}^3$  and a wall thickness of about 0.089 inches. A hot liquid at  $200^\circ$  F.  $(93.3^\circ$  C.) was placed in the cup.

#### Test Results

The temperature measured on the outside wall of the cup was about 140.5° F. (60.3° C.) resulting in drop of about 59.5° F. (33° C.). The maximum temperature over a five-minute period was observed to peak at about 140.5° F. (60.3° C.). The lower the temperature, the better the insulation property of the cup material as the material reduces the heat transferring from the liquid to the cup material exterior.

#### Frangibility

Frangibility can be defined as resistance to tear or punc-  $^{45}$  tures causing fragmentation.

Test Method

The Elmendorf test method described in ASTM D1922-93 was used. The radius of tear was 1.7 inches (43.18 mm).

Test Results

The test results are shown in Tables 3-4 below. The material as formed in one exemplary embodiment of the present disclosure provides superior resistance to tear forces when compared to EPS.

18

TABLE 4

	Summary of Test Res	ults	
	Tear Strength	Sample ID →	Test material cup (mean)
1	Elmendorf Tear machine direction (MD) Arm Elmendorf Tear MD Elmendorf Tear transverse direction (TD) Arm Elmendorf Tear TD	g (gram) gf (gram force) g gf	800 282 800 212
	Tear Strength	Expanded po (mea	
	Elmendorf Tear Arm Elmendorf Tear	800 112	

Note that there was no data obtained for the transverse direction test for expanded polystyrene because expanded polystyrene does not have a material orientation, i.e., a machine or transverse direction, due to the manufacturing process. The range (calculated as: lower range=mean=(3× std dev); upper range=mean+(3× std dev)) for the tested material of the present disclosure was about 213 grams-force to about 351 grams-force in the machine direction and about 143 grams-force to about 281 grams-force in the transverse direction. In comparison, the range of the expanded polystyrene material tested was about 103 grams-force to about 121 grams-force.

Puncture Resistance

Test Method

Determine the force and travel needed to puncture cup sidewall and bottom. An Instron instrument is used in compression mode set to 10 inches (254 mm) per minute travel speed. The cup puncture test fixture on base of Instron is used. This fixture allows the cup to fit over a shape that fits inside the cup with a top surface that is perpendicular to the travel of the Instron tester. The one inch diameter hole of the fixture should be positioned up. The portion of the Instron that moves should be fitted with a 0.300 inch (7.62 mm) diameter punch. The punch with the hole is aligned in the test fixture. The cup is placed over the fixture and the force and travel needed to puncture the cup sidewall is recorded. The sidewall puncture test is repeated in three evenly spaced locations while not puncture testing on the seam of the cup. The bottom of the cup is tested. This should be done in the same manner as the sidewall test except no fixture is used. The cup is just placed upside down on the base of the Instron while bringing the punch down on the center of the cup bottom.

TABLE 3

						7	Test Result	s						
		Machir	ne Directio	on (gram f	orce)				Tra	ınsverse D	irection (g	gram force	e)	
Tag	Test 1	Test 2	Test 3	Test 4	Test 5	mean	std dev.	Test 1	Test 2	Test 3	Test 4	Test 5	mean	std dev.
Test Material	288	262	288	258	315	282	23	232	213	178	205	232	212	23
EPS	108	114	112	116	110	112	3	*						

Specimen#

Specimen#

14

Mean

19

**20** 

Tested Material

Peak

 $Load \; g(f)$ 

Elongation At

Break (mm)

19 3

Elongation At

Break (mm)

10

Test Results	TABLE 6-continued

Results of the typical sidewall puncture and the bottom puncture are shown in Table 5 below.

		10	16859.29	
		Mean	15210.30	
TABLE 5	_	Std. Dev.	1532.83	
	10			
Puncture Test Results	- 10			
Cavity # May Load (lbf) Eyt @ May Load (in)			TABLE 7	

Cavity # Max Load (lbf) Ext. @ Max Load (in)

Expanded polystyrene tested insulative cellular 22.18 0.292 non-aromatic polymeric material (No Rim)

Slow Puncture Resistance—Straw

Test Method

The material as formed in one exemplary embodiment of the present disclosure provides superior resistance to punctures when compared to expanded polystyrene using the Slow Puncture Resistance Test Method as described in ASTM D-3763-86. The test results are shown in Tables 6-9 below.

2936.73 2870.07 10 2572.62 2632.44 20 2809.70 2842.93 2654.55 2872.96 2487.63 10 2866.53 25 2803.25 11 2775.22 12 13 2834.28

Comparison: Expanded Polystyrene

Peak

 $Load \; g(f)$ 

STM 30 Std. Dev.

TABLE 8

Paper Wrapped Expanded Polystyrene

2569.97

2752.06

140.42

Test Results

	Tested Material	
Specimen#	Peak Load g(f)	Elongation At Break (mm)
1	13876.49	_
2	13684.33	_
3	15121.53	_
4	15268.95	17
5	14970.47	20
6	13049.71	_
7	15648.44	17
8	15352.38	23
9	18271.37	_

TADED (

 Specimen#	Peak Load g(f)	Elongation At Break (mm)
1	7930.61	_
2	10044.30	_
3	9849.01	_
4	8711.44	_
5	9596.79	_
6	9302.99	_
7	10252.27	_
8	7785.64	_
9	8437.28	_
10	6751.98	_
11	9993.19	_
Mean	8968.68	_
Std. Dev.	1134.68	_

TABLE 9

Summary of Slow Puncture-Straw Test Results						
Sample ID →	Tested insulative cellular non- aromatic polymeric material cup (mean) grams-force (gf)	Expanded polystyrene (mean) grams- force (gf)	Paper wrapped expanded polystyrene (mean) gram force (gf)			
Average gf:	15210	2752	8969			

#### Example 2

#### Formulation and Extrusion

The following formulation was used:
81.70% Borealis WB140HMS primary polypropylene
0.25% Amco A18035 PPRO talc filled concentrate
2% Ampacet 102823 Process Aid PE MB linear low density polyethylene slip agent

0.05% Hydrocerol CF-40E chemical foaming agent 1% Colortech 11933-19 colorant

15% Braskem F020HC high crystallinity homopolymer polypropylene

3.4 lbs/hour of  $CO_2$  was introduced into the molten resin. Density of the strip formed ranged from about 0.155 g/cm<sup>3</sup> to about 0.182 g/cm<sup>3</sup>.

The formulation was added to an extruder hopper. The  $^{20}$  extruder heated the formulation to form a molten resin mixture. To this mixture was added the  $\mathrm{CO}_2$  to expand the resin and reduce density. The mixture thus formed was extruded through a die head into a strip **82**. The strip was then cut and  $^{25}$  formed into insulative cup **10**.

#### Example 2

#### Test Results

In exemplary embodiments, a tube of extruded insulative cellular non-aromatic polymeric material has two surfaces that are formed under different cooling conditions when the material is extruded. One surface, which will be further referenced as the outside surface of extruded tube, is in contact with air, and does not have physical barriers restricting the expansion. The outside surface of extruded tube surface is cooled by blowing compressed air at cooling rate equal or higher than 12° F. per second. Surface on the opposite side will be referenced as inside of extruded tube. The inside of extruded tube surface is formed when the extruded tube is drawn in the web or machine direction on the metal cooling surface of the torpedo mandrel that is physically restricting 50 the inside of extruded tube and is cooled by combination of water and compressed air at a cooling rate below 10° F. per second. In exemplary embodiments, the cooling water temperature is about 135° F. (57.22° C.). In exemplary embodi- 55 ments, the cooling air temperature is about 85° F. (29.44° C.). As a result of different cooling mechanisms the outside surface of extruded tube and inside of extruded tube surfaces have different surface characteristics. It is known that the 60 cooling rate and method affects the crystallization process of polypropylene altering its morphology (size of crystal domains) and topography (surface profile and smoothness).

An unexpected feature of exemplary embodiments of an extruded sheet as described herein is in the ability of the sheet to form a noticeably smooth, crease and wrinkle free surface,

22

when curved to form a round article, such as cup. The surface is smooth and wrinkle free even inside the cup, where compression forces typically cause material to crush crease easily, especially for low density material with large cell size. In exemplary embodiments, the smoothness of the surface of an extruded sheet of insulative cellular non-aromatic polymeric material as detected by microscopy is such that the depth of the indentations (creases or wrinkles) naturally occurring in the outside and inside of the cup surface when it is subject to extension and compression forces during cup formation may be less than about 100 microns. In one exemplary embodiment, the smoothness may be less than about 50 microns. In one exemplary embodiment, the smoothness may be about 5 microns or less. At about 10 microns depth and less, the micro-wrinkles on cup surface are ordinarily not visible to the naked eye.

In one exemplary embodiment, an insulative cup formed from a sheet comprising a skin and a strip of insulative cellular non-aromatic polymeric material had typical creases (deep wrinkle) about 200 microns deep extending from the top to bottom of the cup. In one exemplary embodiment, an insulative cup formed from a sheet comprising a strip of insulative cellular non-aromatic polymeric material only (without a skin) had typical creases about 200 microns deep extending from top to bottom of the cup. Such creases with depths from about 100 microns to about 500 microns are typically formed when inside of extruded tube is facing inside of the cup in a compression mode. Creases and deep wrinkles may present a problem of unsatisfactory surface quality making final cups unusable or undesirable. Creases may form in instances where sheets include a skin or exclude a skin.

In exemplary embodiments, the insulative cellular non-aromatic polymeric material may be extruded as strip. However microscopy images show that two distinct layers exist within the extruded strip, namely, dull outside extruded tube layer and shiny inside extruded tube layer. The difference between the two layers is in reflectance of the surface due to the difference in crystal domain size. If a black marker is used to color the surface examined by microscope, reflectance is eliminated and the difference between the two surfaces may be minimal or undetectable.

In one exemplary embodiment, a sample strip was prepared without any skin. Black marker was used to eliminate any difference in reflectance between the layers. Images showed that the cell size and cell distribution was the same throughout the strip thickness. A crease of about 200 microns deep was seen as a fold in the surface where the cell wall collapsed under the compression forces.

Differential scanning calorimetry analysis conducted on a TA Instruments DSC 2910 in nitrogen atmosphere showed that with an increase in cooling rate, the crystallization temperature and crystallinity degree decreased for the polymer matrix material of the strip, as shown below in Table 10.

TABLE 10

		Crystallizati	ion of polymer	matrix	
Crystallization temp, in ° C.			C	rystallinity deg	gree, in %
Slow cooling 5° C./min	10° C./ min	Fast cooling 15° C./min	Slow cooling 5° C./min	10° C./ min	Fast cooling 15° C./min
135.3	131.5	129.0	9.2 48.		47.4
Melting	(2 <sup>nd</sup> heat) of	polymer matrix	(heating rate	10° C./min) aft	er crystallization
Melting temp, ° C.				Crystallinity de	egree, %
Slow cooling 5° C./min	10° C./ min	Fast cooling 15° C./min	Slow cooling 5° C./min	10° C./ min	Fast cooling 15° C./min
162.3	162.1	161.8	48.7	47.2	46.9

Differential scanning calorimetry data demonstrates the dependence of crystallization and subsequent 2<sup>nd</sup> heat melting temperature and percent crystallinity on the rate of cooling during crystallization. Exemplary embodiments of a strip of insulative cellular non-aromatic polymeric material may have the melting temperature between about 160° C. (320° F.) and about 172° C. (341.6° F.), crystallization temperature between about 108° C. (226.4° F.) and about 135° C. (275° F.), and percent crystallinity between about 42% and about

In exemplary embodiments the extruded sheet as determined by differential scanning calorimetry at 10° C. per minute heating and cooling rate had a melting temperature of about 162° C. (323.6° F.), crystallization temperature of about 131° C. (267.8° F.) and crystallinity degree of about 35

It was found unexpectedly that the outside extrusion tube surface works favorably in a compression mode without causing appreciable creasing and therefore a cup (or other structure) may advantageously be made with the outside extrusion  $^{40}$ tube surface facing inside of the insulative cup. The difference in the resistance of the inside extrusion tube layer and outside extrusion tube layer to compression force may be due to difference in the morphology of the layers because they were crystallized at different cooling rates.

In exemplary embodiments of formation of an extruded sheet, the inside extrusion tube surface may be cooled by combination of water cooling and compressed air. The outside extrusion tube surface may be cooled by compressed air 50 by using torpedo with circulating water and air outlet. Faster cooling rates may result in the formation of smaller size crystals. Typically, the higher cooling rate, the greater the relative amount of smaller crystals that is formed. X-Ray diffraction analysis of an exemplary extruded sheet of insu- 55 period was observed to peak at about 151° F. (66.1° C.). lative cellular non-aromatic polymeric material was conducted on Panalytical X'pert MPD Pro diffractometer using Cu radiation at 45 KV/40 mA. It was confirmed that the outside extrusion tube surface had a crystal domain size of about 99 angstrom, while the inside extrustion tube surface 60 had a crystal domain size of about 114 angstrom. In exemplary embodiments, an extruded strip of insulative cellular non-aromatic polymeric material may have a crystal domain size below about 200 angstroms. In exemplary embodiments, an extruded strip of insulative cellular non-aromatic poly- 65 meric material may have a crystal domain size preferably below about 115 angstroms. In exemplary embodiments, an

extruded strip of insulative cellular non-aromatic polymeric material may have a crystal domain size below about 100 angstroms.

Rigidity

Test Method

The test method is the same as described for rigidity testing in Example 1.

Test Results

The rigidity test results are shown in Table 11 below.

TABLE 11

		unlidded/filled 200° F. Rigidities (kg's)		110000	/filled 2 dities (I				
5	Sam- ple#	Seam	90° from Seam	Aver- age	Seam	90° from Seam	Aver- age	Gram Weights	Wall Thick- ness
	B1	0.354	0.380	0.367	0.470	0.528	0.499	12.6	0.0744
	B2	0.426	0.464	0.445	0.598	0.610	0.604	13.0	
	В3	0.526	0.494	0.510	0.628	0.618	0.623	12.4	
)	B4	0.592	0.566	0.579	0.740	0.746	0.743	13.2	
				0.475			0.617	12.80	
									Density
									0.1817

#### 45 Insulation

Test Method—Wall Temperature

An insulative cup formed from the formulation noted above was used having a density of about 0.18 g/cm<sup>3</sup> and a wall thickness of about 0.074 inches (1.8796 mm). A hot liquid at 200° F. (93.3° C.) was placed in the cup.

Test Results

The temperature measured on the outside wall of the cup was about 151° F. (66.1° C.) with a drop of about 49.0° F. (27.2° C.). The maximum temperature over a five-minute

Insulation testing in the form of thermal conductivity was

Test Method—Thermal Conductivity

This test measures bulk thermal conductivity (W/m-K), measured at ambient temperature and at 93° C. (199.4° F.). A TherinTest TPS 2500 S Thermal Constants Analyzer instrument was used, employing the test method of ISO/DIS 22007-2.2 and using the Low Density/High Insulating option. The TPS sensor #5501 0.2521 inch radius (6.403 mm radius) with Kapton® insulation was used for all measurements. A 20 second test was done, using 0.02 Watts power. Data using points 100-200 were reported.

Test Results

The test results are shown in Table 12 below.

TABLE 12

Mean Thermal Conductivity Results				
Temp. (° C.)	Mean Thermal Conductivity (W/m-K)	Standard Deviation (W/m-K)		
21 93	0.05792 0.06680	0.00005 0.00025	10	

Although only a number of exemplary embodiments have been described in detail above, those skilled in the art will readily appreciate that many modifications are possible in the 15 exemplary embodiments without materially departing from the novel teachings and advantages. Accordingly, all such modifications are intended to be included within the scope of this disclosure as defined in the following claims.

As used in the specification and the appended claims, the singular forms "a," "an" and "the" include plural referents unless the context clearly dictates otherwise. Ranges may be expressed herein as from "about" one particular value, and/or to "about" another particular value. When such a range is expressed, another embodiment includes from the one particular value and/or to the other particular value. Similarly, when values are expressed as approximations, by use of the antecedent "about," it will be understood that the particular value forms another embodiment. It will be further understood that the endpoints of each of the ranges are significant both in relation to the other endpoint, and independently of the other endpoint.

"Optional" or "optionally" means that the subsequently described event or circumstance may or may not occur, and that the description includes instances where said event or 35 circumstance occurs and instances where it does not.

Throughout the description and claims of this specification, the word "comprise" and variations of the word, such as "comprising" and "comprises," means "including but not limited to," and is not intended to exclude, for example, other 40 additives, components, integers or steps. "Exemplary" means "an example of" and is not intended to convey an indication of a preferred or ideal embodiment. "Such as" is not used in a restrictive sense, but for explanatory purposes.

Disclosed are components that can be used to perform the disclosed methods, equipment, and systems. These and other components are disclosed herein, and it is understood that when combinations, subsets, interactions, groups, etc. of these components are disclosed while specific reference of each various individual and collective combinations and permutation of these may not be explicitly disclosed, each is specifically contemplated and described herein, for all methods, equipment and systems. This applies to all aspects of this application including, but not limited to, steps in disclosed methods. Thus, if there are a variety of additional steps that 55 can be performed it is understood that each of these additional steps can be performed with any specific embodiment or combination of embodiments of the disclosed methods.

It will be apparent to those skilled in the art that various modifications and variations can be made without departing from the scope or spirit. Other embodiments will be apparent to those skilled in the art from consideration of the specification and practice disclosed herein. It is intended that the specification and examples be considered as exemplary only.

It should further be noted that any publications and brochures referred to herein are incorporated by reference in their entirety. The invention claimed is:

- 1. A formulation for forming an insulative cellular non-aromatic polymeric structure, the formulation comprising
  - a first polymer material comprising at least one high melt strength polypropylene having a melt strength of at least 36 and a melting temperature of at least 163° C. (325.4° F.).
  - a second polymer material comprising at least one polymer selected from the group consisting of polypropylene, polyethylene, and mixtures thereof,
  - at least one nucleating agent selected from the group consisting of chemical nucleating agents, physical nucleating agents, and combinations and mixtures thereof, and at least one blowing agent.
- 2. The formulation of claim 1, wherein the second polymer material is a homopolymer.
- 3. The formulation of claim 2, wherein the first polymer material is a homopolymer.
- **4**. The formulation of claim **3**, wherein the insulative cellular non-aromatic polymeric structure has a density in a range of about  $0.01 \text{ g/cm}^3$  to about  $0.19 \text{ g/cm}^3$ .
- 5. The formulation of claim 4, further comprising at least one slip agent.
- **6**. The formulation of claim **4**, wherein the insulative cellular non-aromatic polymeric structure has a density in a range of about 0.05 g/cm<sup>3</sup> to about 0.19 g/cm<sup>3</sup>.
- 7. The formulation of claim 1, wherein the structure has cells having an average cell aspect ratio in at least one direction in a range of about 1.0 to about 3.0.
- **8**. The formulation of claim **7**, wherein the structure has cells having an average cell aspect ratio in at least one direction of about 2.0.
- 9. The formulation of claim 8, wherein the insulative cellular non-aromatic polymeric structure has a density in a range of about 0.05 g/cm<sup>3</sup> to about 0.19 g/cm<sup>3</sup>.
- 10. The formulation of claim 9, further comprising at least one slip agent.
- 11. The formulation of claim 1, wherein the first polymer material is a homopolymer.
- 12. The formulation of claim 11, wherein the structure has cells having an average cell aspect ratio in at least one direction of about 2.0.
- 13. The formulation of claim 12, wherein the insulative cellular non-aromatic polymeric structure has a density in a range of about 0.05 g/cm<sup>3</sup> to about 0.19 g/cm<sup>3</sup>.
- 14. The formulation of claim 13, further comprising at least one slip agent.
- 15. A formulation for forming an insulative cellular non-aromatic polymeric structure, the formulation comprising
  - a first polymer material comprising at least one high melt strength polypropylene having a melt strength of at least 36 and a melting temperature of at least 163° C. (325.4° F.),
  - a second polymer material comprising at least one polypropylene selected from the group consisting of impact copolymers and high crystalline homopolymers,
  - at least one nucleating agent selected from the group consisting of chemical nucleating agents, physical nucleating agents, and combinations thereof, and
  - at least one blowing agent comprising at least one composition selected from the group consisting of chemical blowing agents, inert gases, and combinations thereof.
- 16. The formulation of claim 15, wherein the structure has cells having an average cell aspect ratio in at least one direction of about 2.0.

- 17. The formulation of claim 16, wherein the insulative cellular non-aromatic polymeric structure has a density in a range of about 0.05 g/cm<sup>3</sup> to about 0.19 g/cm<sup>3</sup>.

  18. The formulation of claim 17, further comprising a slip
- agent.
- 19. The formulation of claim 15, wherein the first polymer material is a homopolymer.
- 20. The formulation of claim 19, further comprising at least one slip agent.

10